



# Recent advances of ammonia synthesis under ambient conditions over metal-organic framework based electrocatalysts

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## ABSTRACT

Ammonia (NH<sub>3</sub>) is an essential chemical and a promising fuel, but its industrially produced process is carbon-intensive and highly energy-consuming. Developing a green and sustainable NH<sub>3</sub> synthesis route is extremely urgent. Electrochemical ammonia synthesis (EAS) powered by renewable electricity energy under ambient conditions is fascinating, while exploring the efficient electrocatalysts and suitable nitrogen source is critical. Due to the unique characteristics of adjustable porosity and component, large specific surface area and diverse structure, metal-organic frameworks (MOFs) and their various derivatives have captured immense interest in EAS. Herein, the advance in EAS via electrocatalytic reduction reactions (ERRs) from various nitrogen source under ambient conditions over MOF-based electrocatalysts is timely summarized, aiming to offer a deep insight to the structure-activity relationship of MOF-based electrocatalysts for EAS. Current challenges and future prospects for EAS are proposed at the end of this review as well.

## 1. Introduction

Ammonia (NH<sub>3</sub>) is a vital chemical in agricultural and industrial applications, such as fertilizer, pharmaceutical, and chemical production [1], as well as a potential hydrogen energy carrier due to the high hydrogen mass fraction (17.5 wt%), zero carbon content and much higher liquefaction temperature (−33 °C) [2,3]. Currently, the global NH<sub>3</sub> production is close to 200 million metric tons, which highly relies on the traditional Haber-Bosch (H-B) process [4]. However, this process requires high temperature (300–500 °C) and high pressure (150–300 atm) to break the highly inert N≡N triple bond, which consumes 1–2% of worldwide energy consumption along with over 1% of the world's greenhouse gas emission [5–7]. Additionally, large and centralized plant infrastructure of H-B process limits the location of NH<sub>3</sub> plants. Thus, it is urgently needed to exploit a sustainable, distributed and environmentally friendly process as an alternative to the traditional H-B process.

Electrochemical ammonia synthesis (EAS) driven by the renewable electricity energy under ambient conditions is an attractive strategy for green NH<sub>3</sub> synthesis in small-scale devices [8–14]. Recently, many efforts have been made to synthesize NH<sub>3</sub> from abundant nitrogen (N<sub>2</sub>) under aqueous conditions via electrocatalysis [15–19]. However, the

yield of NH<sub>3</sub> is far from the demand of industrial requirements due to the poor water solubility and high bond energy (941 kJ mol<sup>−1</sup>) of N<sub>2</sub> as well as the competitive hydrogen evolution reaction (HER) during the electrocatalytic process [20]. Some strategies have been adopted to improve the yield and selectivity of NH<sub>3</sub>. For example, to avoid the dissolution issues of N<sub>2</sub> and competitive HER, a case in point is electrochemical lithium-mediated N<sub>2</sub> reduction reaction (Li-NRR) in nonaqueous electrolytes [21–23]. During the Li-NRR, Li<sup>+</sup> is first reduced to metallic Li, which then spontaneously reacts with N<sub>2</sub> to generate nitrogenous lithium compound; subsequently, the nitrogenous lithium compound is converted into NH<sub>3</sub> with proton sources through electrocatalysis [24]. Another promising strategy is developing oxynitrides (e.g., nitrate (NO<sub>3</sub><sup>−</sup>), nitrite (NO<sub>2</sub><sup>−</sup>) and gaseous nitrogen dioxides (NO<sub>x</sub>)) as nitrogen source instead of N<sub>2</sub> due to the following reasons: 1) the lower N = O bond energy (204 kJ mol<sup>−1</sup>) and higher solubility make it easier for the adsorption and activation of these oxynitrides than N<sub>2</sub>, which can significantly increase the yield and selectivity of NH<sub>3</sub>; 2) these oxynitrides as environmental pollutants are excessive in groundwater and atmosphere with the development of industry and agriculture, so that electrochemical conversion of these oxynitrides pollutants to high-value NH<sub>3</sub> can achieve “turn waste into wealth” [25–30]. Regardless of the

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development of the various strategies, efficient electrocatalysts are the core of EAS. Developing the advanced electrocatalytic materials with abundant active sites, good adsorption capacity and high stability for efficient and stable  $\text{NH}_3$  synthesis is crucial but greatly challenging.

Metal-organic framework (MOF) is a class of crystalline organic-inorganic hybrid functional porous material, which is assembled by metal ions/clusters and organic linkers [31,32]. Due to their unique adjustable porosity and component, large specific surface area and diverse structure, MOF-based materials have been prepared and employed in diverse electrocatalytic fields, such as HER [33–36], oxygen evolution reaction (OER) [37–39],  $\text{CO}_2$  reduction reaction [40–42] and  $\text{NH}_3$  synthesis [43–45]. Furthermore, MOFs are ideal precursors to acquire functionalized MOFs derivatives like metal oxides, porous carbon or metal/carbon composites through pyrolysis, which represents an efficient strategy for the preparation of outstanding electrocatalytic materials [39,46,47]. Apart from the common merits with MOFs, MOF derivatives also demonstrate the following advantages: (1) MOF derivatives usually show enhanced stabilities compared with MOFs in electrocatalysis due to no break of coordination bonds or organic linkers; (2) Profiting from the formation of carbon after high-temperature pyrolysis, they show improved electrical conductivity; (3) Both metallic and non-metallic elements can participate in the formation of MOF derivatives, which may act as active sites for electrocatalysis. By virtue of the above advantages, various MOF-based materials have been developed as electrocatalysts in the past years [48–50]. To date, the EAS using MOF-based materials as electrocatalysts are still in the preliminary stage and few reviews have focused attention to summarize MOF based materials towards EAS [51]. Therefore, a timely summary and comprehensive review on the structure-activity relationship are conducive to develop superior MOF-based catalysts in the field of EAS.

In this review, we summarize recent progress of  $\text{NH}_3$  synthesis from various nitrogen sources under ambient conditions over MOF-based electrocatalysts (Scheme 1). The mechanism of EAS via ERRs using various nitrogen sources as well as the quantification methods of ammonia are firstly analyzed and discussed in detail. Then we discuss the structural features and merits of MOF-based materials acted as electrocatalysts. Subsequently, recent advance in  $\text{NH}_3$  synthesis from various nitrogen sources under ambient conditions over MOF-based electrocatalysts including pristine MOFs/MOF composites and MOF derivatives is summarized, and the effect of composition, structure and electronic properties of MOF-based electrocatalysts on the performance of EAS is analyzed and discussed. Finally, current challenges and future prospects of EAS are proposed. We believe that this review will provide the scientific guidance to explore the innovations of MOF-based materials for  $\text{NH}_3$  synthesis.

## 2. Mechanism of EAS using various nitrogen sources and ammonia quantification

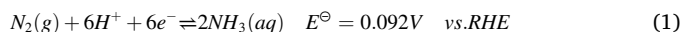
### 2.1. Mechanism of EAS using various nitrogen sources

For EAS,  $\text{N}_2$ , one of the main components of the atmosphere, is theoretically and experimentally studied as the feedstock by numerous researchers. In addition, the natural N cycle has been severely altered by the modern human activities, such as the excessive use of fertilizers and industrial production, which result in the deposition of undesired nitrogenous pollutants ( $\text{NO}_3^-/\text{NO}_2^-$ , gaseous  $\text{NO}_x$ , etc.) from the environment. Compared with the inert  $\text{N}_2$ , the nitrogenous pollutants are reactive N and can be thermodynamically easier to be reduced. Herein, we give an insight to the ERRs for EAS from various nitrogen sources.

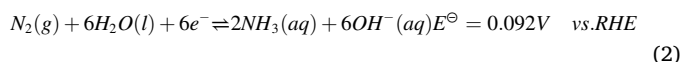
#### 2.1.1. $\text{N}_2$ reduction reaction (NRR)

Compared to the traditional H-B process, the electrocatalytic NRR to produce  $\text{NH}_3$  under mild conditions can enable distributed  $\text{NH}_3$  production using renewable electricity, reduce carbon emissions, ease the reactor design, and simplify the complexity of  $\text{NH}_3$  production plants [17,52–54]. In the electrolytic cell, the NRR proceeds on the surface of cathode, which can be simply described as follows:  $\text{N}_2$  molecules in the electrolyte are first adsorbed on electrode surface and then activated by the electrons supplied from external circuit along with stepwise hydrogenation to form  $\text{NH}_3$ . The half-reaction electrochemical NRR into  $\text{NH}_3$  involves six electrons coupled protons transfer reactions and the corresponding equilibrium potentials versus reversible hydrogen electrode (vs. RHE) are as follows [52,55,56]:

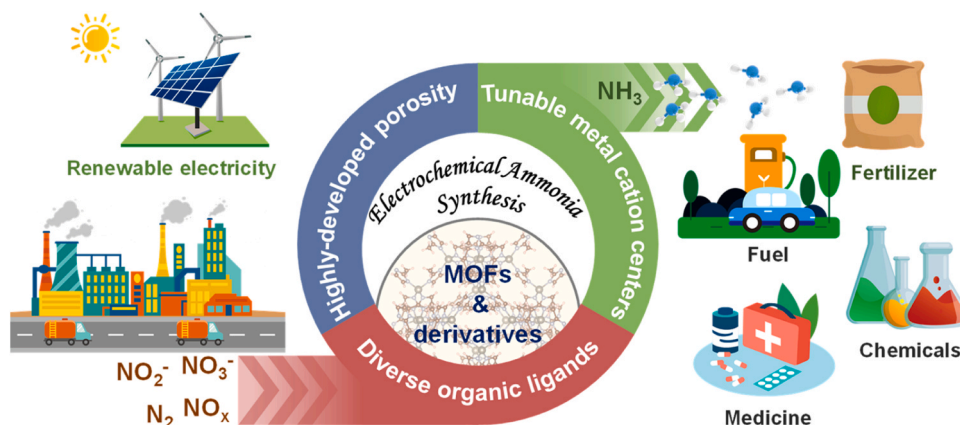
Acidic media:



Basic media:

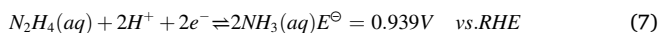
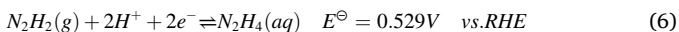
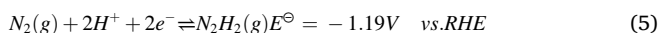
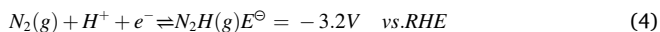
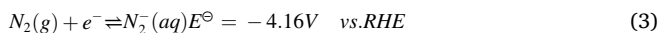


From the point of the theoretical equilibrium potentials, the NRR can occur at room temperature and atmospheric pressure when an adequately negative potential is applied to an electrode [57]. Even so, the energy gap between the lowest unoccupied molecular orbital and the highest occupied molecular orbital of  $\text{N}_2$  is up to 10.82 eV, indicating the great difficulty in the first-step activation of  $\text{N}_2$  by electron, which corresponds to the much negative equilibrium potentials of 1  $\text{e}^-$  reduction (Equation 3) [58,59]. What's more, the NRR into  $\text{NH}_3$  is performed through multi-step proton-electron transfer reactions and multiple intermediates are involved (Equations 4–7), in which the redox potential for the formation of the  $\text{N}_2\text{H}$  intermediate is also much negative, suggesting the difficulty of the first H atom addition. Additionally,



Scheme 1. Scheme of EAS from various nitrogen source.

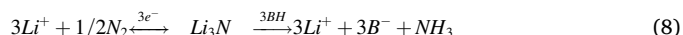
considering the equilibrium potential of HER (0.00 V vs. RHE) is similar to that of NRR, the competition of HER in aqueous solutions is unavoidable. Thus, even though the EAS from NRR is thermodynamically favored, large barriers associated with the first activation and reduction processes to form favorable intermediate species and strong competition reaction of HER must be circumvented through effective catalyst design.



Electrolyte is an essential part for the electrochemical NRR to  $\text{NH}_3$ . In the past decades, various types of electrolytes including both solid and liquid electrolyte have been used in electrochemical cells for  $\text{NH}_3$  synthesis, which are operated in a wide temperature range. According to the operating temperature, the electrochemical experiments studies can be classified as: high temperature ( $T > 500^\circ\text{C}$ ), intermediate temperature ( $500^\circ\text{C} > T > 100^\circ\text{C}$ ) and low temperature ( $T < 100^\circ\text{C}$ ) [60]. In the high temperature range, solid-state proton ( $\text{H}^+$ ) or oxygen-ion ( $\text{O}^{2-}$ ) conductors, such as perovskites or materials with fluorite or pyrochlore structures, and suitable carbonates were developed as the electrolyte materials [61,62]. The mobile charge carriers in these electrolytes which ensure the circulation of the current circuit are usually  $\text{H}^+$  or  $\text{O}^{2-}$  ion. And we can depict the reactor-cell design, electrode reactions and mobile charge carriers in these electrolytes as Fig. 1a, b. For the intermediate temperature range, molten salts (like chlorides, hydroxides), solid acids or the composite materials of solid oxides mixed with alkali metal salts were usually used as electrolyte [63–65]. Notably, in some reported alkali metal molten salts electrolytes,  $\text{N}_2$  reacted with alkali metal and dissolved to nitride ions ( $\text{N}^{3-}$ ), and the  $\text{N}^{3-}$  can also act as the charge carriers in the electrolysis process. The mobile  $\text{N}^{3-}$  in these electrolytes can be depicted as Fig. 1c. In the low temperature range, aqueous solutions, ionic liquids and polymer membranes were most commonly employed as the electrolytes, and  $\text{H}^+$  ion or hydroxide ( $\text{OH}^-$ ) ion usually

acted as the charge carriers [66]. Fig. 1d shows a schematic diagram of  $\text{NH}_3$  synthesis in the electrochemical cell using  $\text{OH}^-$  ion conducting electrolytes. Even though diverse electrolytes with different ion conductors have been explored for EAS via NRR, the conductivity of proton-conducting electrolytes in low temperature, such as Nafion, is much higher than of those of other ion conductors. Unfortunately, the reaction kinetics of  $\text{NH}_3$  synthesis from  $\text{N}_2$  are quite slow at low temperatures, which urgently need us to develop more efficient reactors and catalysts.

Apart from the direct hydrogenation of  $\text{N}_2$  to  $\text{NH}_3$ , mediators (including lithium (Li), transition-metal compounds, metal-free complexes, and enzymes) have also been investigated as a bridge to not only circumvent the competitive HER but convert  $\text{N}_2$  to  $\text{NH}_3$  under ambient conditions. Among the mediator-strategies, the lithium-mediated high-efficiency electro-ammonia synthesis technology is expected to become an industrialized EAS technology due to metal Li can spontaneously react with nitrogen at room temperature and normal pressure. The proposed mechanism can be described as Equation 8 [67]:



In the electrochemical synthesis process, Li metal first spontaneously reduces  $\text{N}_2$  under ambient conditions to produce lithium nitride ( $\text{Li}_3\text{N}$ ). Then,  $\text{Li}_3\text{N}$  reacts with a suitable proton carrier (BH) to generate ammonia and liberate  $\text{Li}^+$  to restart the electrocatalytic cycle (Fig. 2) [24,68]. In 1993, Tsuneto et al. first carried out the electrochemical Li-mediated  $\text{NH}_3$  synthesis using a single-compartment electrochemical cell equipped with a platinum anode and a metal cathode (Al, Ti, Mo, Fe, Co, Ni, Cu, Ag, Zn, and Pb) [69]. The electrolyte was tetrahydrofuran (THF) containing 0.2 M  $\text{LiClO}_4$  and 0.18 M ethanol as proton source. In recent years, this idea has also been demonstrated experimentally by some researchers, and the current-to- $\text{NH}_3$  efficiency even closely approaching 100%. Nonetheless, the drawbacks that the high reduction potential required for electrochemical lithium cycle, lithium loss and safety issues related to handling the highly reactive metal Li exist and may block the application of the Li-mediated strategies at industrial scales, which need researchers overcome the technical barriers.

Recently, considering that direct conversion of  $\text{N}_2$  to  $\text{NH}_3$  either by H-B process or electrochemical NRR has practical drawbacks, two-step

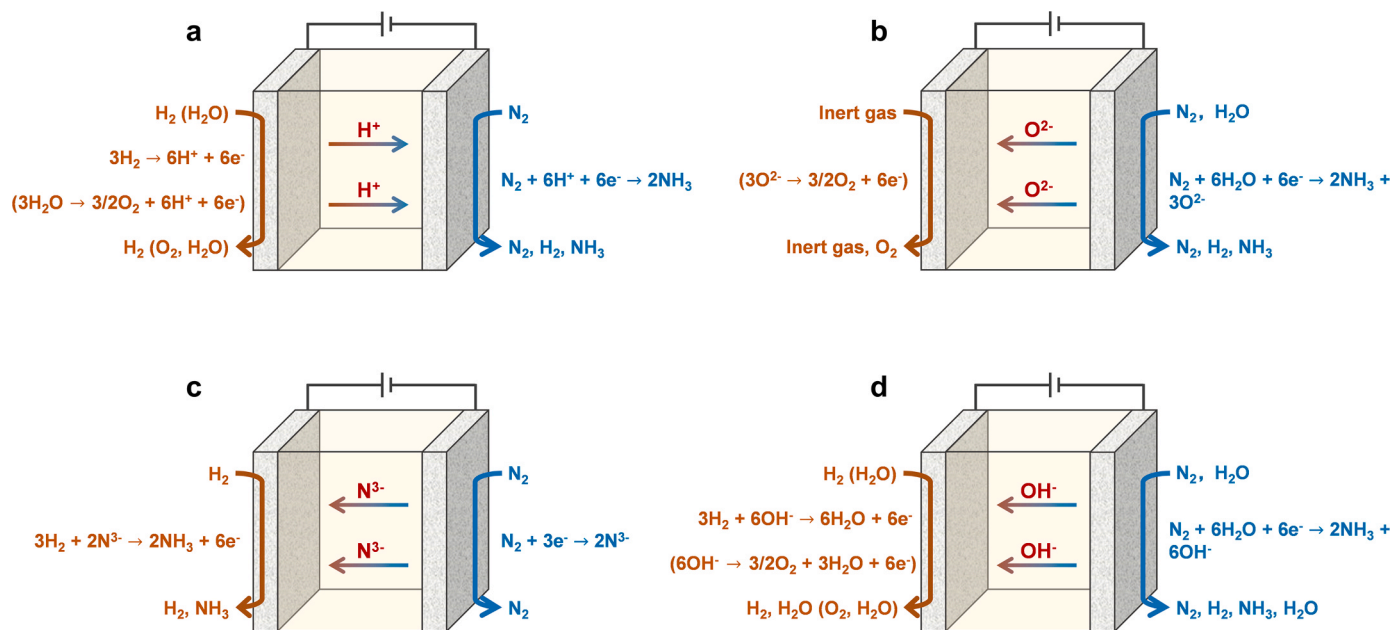


Fig. 1. Electrode reactions for  $\text{NH}_3$  synthesis in electrochemical cells using (a) proton ( $\text{H}^+$ ), (b) hydroxide ion ( $\text{OH}^-$ ), (c) oxide ion ( $\text{O}^{2-}$ ), and (d) nitride ion ( $\text{N}^{3-}$ ) conducting electrolytes.

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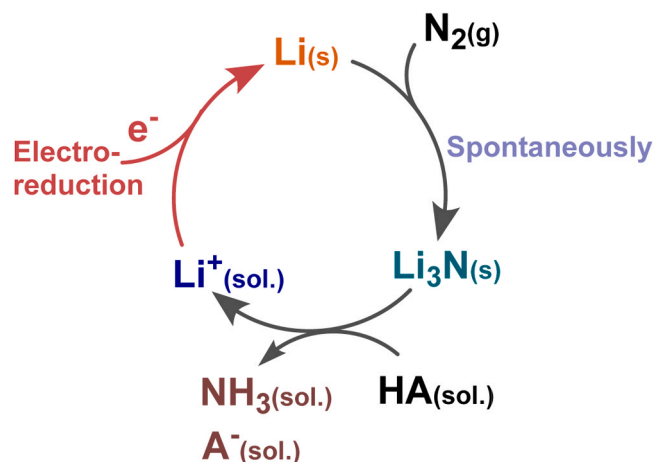


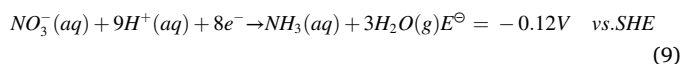
Fig. 2. The cycle of Li-mediated ammonia synthesis. Reproduced with permission [24]. Copyright 2019 Elsevier.

process for  $NH_3$  synthesis using  $N_2$  as the feedstock has been explored. The innovative idea is that we can first convert the sluggish  $N_2$  into more reactive species (such as nitrogen oxanions) by eco-friendly and economical approach, which are then reduced to  $NH_3$  through effective process. For example, Qiao et al. first employed the low-cost air and water as feedstocks for scale-up  $NH_3$  synthesis under ambient conditions through two steps: (1)  $N_2$  oxidation to  $NO_x^-$  by a facile plasma technique (pNOR) and (2) selectively electrocatalytic  $NO_x^-$  reduction ( $NO_x^-$ RR) to  $NH_3$  (Fig. 3a) [70]. In the first plasma-driven  $N_2$  oxidation step, the total  $NO_x^-$  yield can reach ca.  $1.35 \text{ mmol h}^{-1}$ . Then, the surface boron-rich core-shell nickel boride nanoparticle ( $Ni_3B@NiB_{2.74}$ ) was developed as electrocatalyst to achieve ca. 100% conversion of as-obtained  $NO_x^-$  to  $NH_3$ . Additionally, Wu and co-workers demonstrated cobaloximes as a bioinspired molecular platform for EAS via electrocatalytic  $NO_x^-$ RR coupled with plasma-driven  $N_2$  oxidation (Fig. 3b) [71]. Qiu's group used Cu nanoparticles (NPs) as a representative electrocatalyst to systematically investigated the plasma-enabled activation and recombination processes of  $N_2$  and  $O_2$  molecules as well as the mechanism of  $eNO_x^-$ RR at a microscopic level (Fig. 3c) [72]. The pNOR- $eNO_x^-$ RR system is showed in Fig. 3d, in which  $N_2$  and  $O_2$  are first activated and converted into NOx species by the spark discharge, and then the  $NO_x^-$  ions are electrochemically reduced to  $NH_3$  over Cu NPs. As shown in Fig. 3e, the concentrations of  $NO_2^-$ ,  $NO_3^-$ , and  $NO_x^-$  gradually increase with the increase of spark discharge time. Accordingly, the  $NH_3$  partial current density presents a rising tendency as the spark discharge time prolongating, suggesting the promotion effect of the spark discharge process on  $NH_3$  synthesis (Fig. 3f). The strategy of "oxidation followed by reduction" provides new avenue and insight of renewable chemicals production by integrating various advanced technologies.

### 2.1.2. $NO_3^-/NO_2^-$ reduction reaction ( $NO_3^-$ RR/ $NO_2^-$ RR)

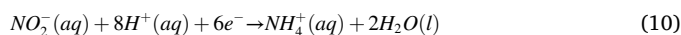
Influenced by excessive anthropogenic activities, including the overuse of nitrogen-based fertilizers and the massive emission of industrial and domestic sewage, the amount of  $NO_3^-$  in surface water and underground is seriously excessive, threatening the human health [73]. As discussed in Introduction,  $NO_3^-$  is easier to activate and absorb on the electrode surface than  $N_2$ , so that it is great meaningful and promising to use the green electricity to drive  $NO_3^-$  reduction reaction to value-added  $NH_3$ , which not only alleviates the environmental issues but also turns waste into wealth (Fig. 4) [74–77]. Considering the dissolved  $NH_4^+$  can be easily collected using membrane separation technology or by heating distillation separation [78,79], the strategy of electrocatalytic  $NO_3^-$ RR for ammonia synthesis also can easily integrate with some mature industrial technologies, indicating its potential compatibility and flexibility towards scale up applications [80].

The reaction equation of electrochemical  $NO_3^-$ RR into  $NH_3$  can be described as Equation 9, where SHE is the abbreviation of standard hydrogen electrode [81]:



While  $NO_3^-$ RR is a complicated and multi-step electron reduction and hydrogenation process, which involves the nitrogen-containing intermediate species from +5 to -3 valence states. As for the electrocatalytic mechanism, two pathways have been proposed by M.T.M. Koper: indirect reduction and direct reduction [82]. The indirect reduction of  $NO_3^-$  is an autocatalytic procedure, in which  $NO_3^-$  itself does not participate in the electron-transfer process but other intermediate species can be involved in the electron transfer reaction. The indirect reduction mechanism is experimentally verified only in the highly acidic environments ( $> 1.0 \text{ M}$ ) with high  $NO_3^-$  concentration ( $> 1.0 \text{ M}$ ) and at low overpotentials (0.8–0.9 V vs. SHE). The direct electroreduction of nitrate can be described as follows: (1)  $NO_3^-$  is stepwise reduced by the adsorbed active hydrogen atom ( $H_{ads}^*$ ), which is generated from  $H_2O$  reduction by electron on the cathode surface, and the intermediates species may be  $NO_2^-$ ,  $NO_{ads}$ ,  $N_{ads}$ ,  $NH_{ads}$ ,  $NH_2$ , and so on; (2)  $NO_3^-$  reacts with the electrons on cathode surface and is simultaneously hydrogenated by  $H^+$  in the electrolyte (Fig. 5) [81]. When the  $NO_3^-$  is at low concentrations (below 0.1 M), the direct reduction mechanism may mainly execute. During the electron/ $H^+$  reduction mechanism, the reduction of  $NO_3^-$  to  $NO_2^-$  is the rate-determining step and the reaction rate is directly affected by the adsorption capacity of  $NO_3^-$  on the electrocatalysts surface. Additionally,  $NO_{ads}$  is the divergent center towards  $N_2O$ ,  $N_2$ , and  $NH_3$  product, suggesting the subsequent electroreduction pathway of  $NO_{ads}$  determine the selectivity of  $NO_3^-$ RR to  $NH_3$  [83]. Thus, the ideal electrocatalyst should not only better adsorb and activate  $NO_3^-$  but also functionally electro-reduce  $NO_{ads}$  to  $NH_3$ .

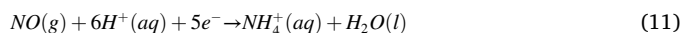
Apart from  $NO_3^-$ ,  $NO_2^-$  is the most common N-contaminant in the aquatic ecosystem, which threatens the survival of organisms. In recent years, researchers also have employed  $NO_2^-$  as the nitrogen source for EAS [71,85–87]. Similarly, electrocatalytic  $NO_2^-$ RR involves complex six electrons transfer and multi-step hydrogenation process described as Equation 10 (Fig. 6) [84].



Thus, the challenge that controlling the selectivity of desired product urges researchers to develop effective reaction systems with high efficiency and specificity for electrochemical  $NO_2^-$ RR.

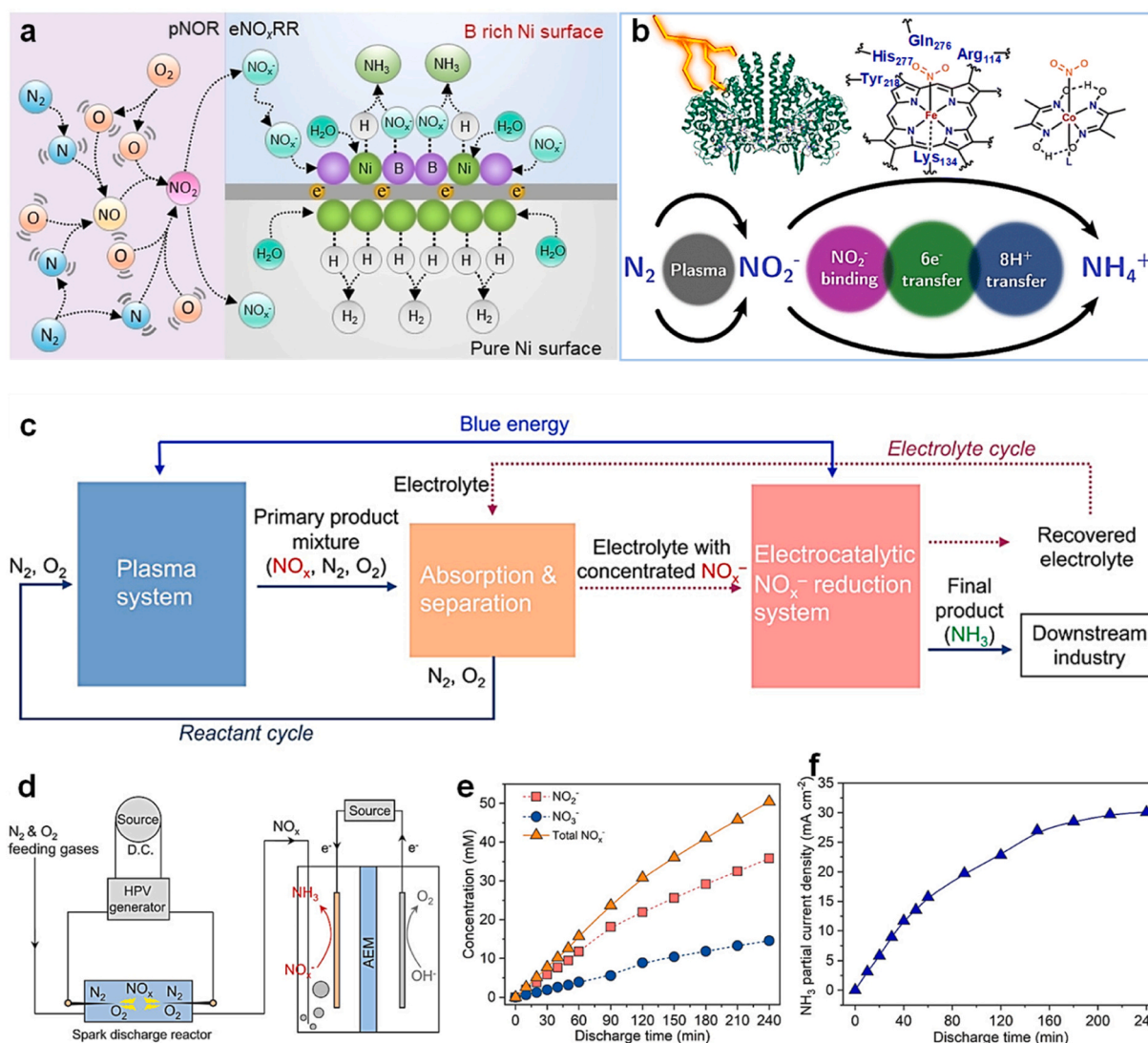
### 2.1.3. Gaseous $NO_x$ reduction reaction ( $NO_x$ RR)

Gaseous  $NO_x$  ( $NO$  and  $NO_2$ , etc.) are important air pollutants that can cause severe environmental issues, such as acid rain, photochemical smog, and so on [88]. It is estimated that about 53 million tons of nitrogen oxides are emitted in the atmosphere by human activities (industrial production, motor vehicle exhaust, etc.) worldwide every year. Currently, the mature strategies for the reduction of  $NO_x$  can be summarized as two kinds: reducing  $NO_x$  emission by optimizing the general combustion process and selective catalytic reduction of  $NO_x$  into non-toxic  $N_2$  [89]. Both the two methods are less economical than recently proposed strategy that  $NO_x$  reduction to  $NH_3$  using the renewable energy, which not only eliminates the toxic  $NO_x$  contaminant in the air but also synthesizes high value-added  $NH_3$  (Fig. 7) [90]. Since nitric oxide ( $NO$ ) is the only insoluble nitrogen oxide, researchers pay more attention to designing efficient electrocatalysts for  $NO$  reduction to  $NH_3$ . The total reaction formula of electrocatalytic  $NO$  reduction reaction (NORR) to  $NH_3$  can be described as Equation 11 [91]:



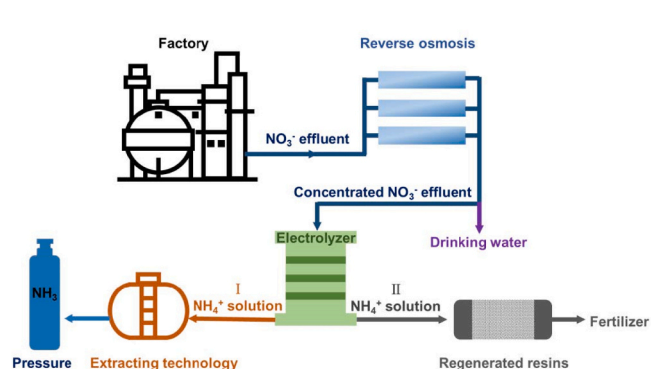
For the reaction mechanism of NORR, two main pathways were proposed: (1)  $NO \rightarrow NO^* \rightarrow NOH^* \rightarrow HNOH^* \rightarrow NH^* \rightarrow NH_2^* \rightarrow NH_3$





**Fig. 3.** (a) The pNOR + eNO<sub>x</sub>RR process and dual-site mechanism for boosted eNO<sub>x</sub>RR activity, (b) NH<sub>3</sub> synthesis via NO<sub>2</sub><sup>-</sup> by natural cytochrome c nitrite reductase and cobaloxime electrocatalysts. (c) Illustration for the proposed pNOR-eNO<sub>x</sub>RR process integration system. (d) Illustration for the plasma-enabled cascade pNOR-eNO<sub>x</sub>RR integrated system, (e) Concentrations of NO<sub>2</sub><sup>-</sup>, NO<sub>3</sub><sup>-</sup>, and total NO<sub>x</sub><sup>-</sup> as a function of spark discharge time, (f) NH<sub>3</sub> partial current density as a function of spark discharge time in the range of 0–240 min.

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**Fig. 4.** The schematic illustration for incorporating nitrate-to-ammonia technique into present technological processes.

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\* → NH<sub>4</sub><sup>+</sup> and (2) NO → NO\* → NOH\* → N\* → NH\* → NH<sub>2</sub>\* → NH<sub>3</sub> → NH<sub>4</sub><sup>+</sup>, both where the adsorbed NOH\* is the pivotal intermediate [90,92].

## 2.2. Methods of ammonia quantification

The accurate detection and quantification of NH<sub>3</sub> are crucial for evaluating the performance of EAS. So far, several analysis methods are commonly used including colorimetric method, ion chromatography (IC) method, ammonia ion-selective electrode and <sup>1</sup>H NMR spectroscopy method, and the assess of partial common techniques can be seen in Fig. 8 [93]. Some other methods, such as fluorometric method [94,95], conductivity method [96], titrimetric method [97], and enzymatic method [98], can also quantify the dissolved NH<sub>3</sub> concentration but less used in the electrochemical ammonia field.

Colorimetric method is the most common detection method used in the laboratory due to the low cost and its high precision, mainly including three categories: Nessler's reagent method, indophenol blue method and salicylate method. Firstly, the Nessler's reagent, developed

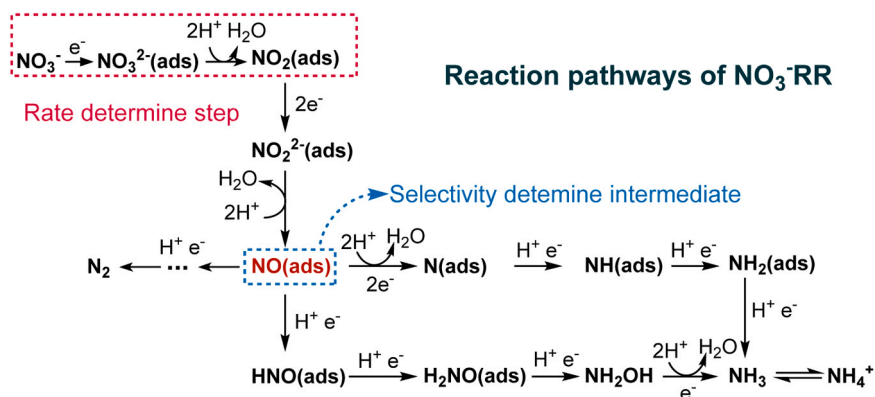


Fig. 5. Schematic illustration of reaction pathways for  $\text{NO}_3^-$  reduction over electrocatalysts. Reproduced with permission [81]. Copyright 2021, Royal Society of Chemistry.

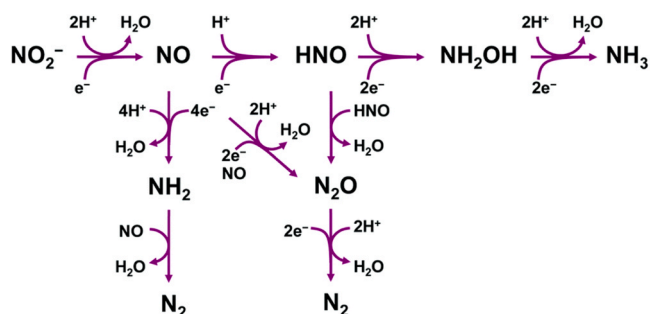


Fig. 6. The pathway of electrochemical  $\text{NO}_2^-$ RR to different products. Reproduced with permission [84]. Copyright 2022, Royal Society of Chemistry.

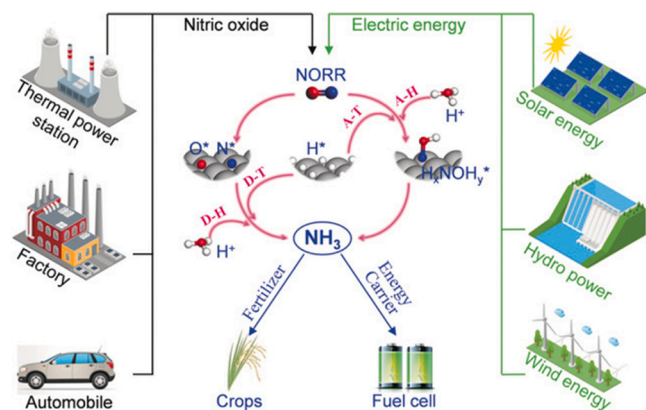


Fig. 7. Illustration of the proposed EAS route from NO. Reproduced with permission [90]. Copyright 2020, Wiley-VCH.

by Julius Nessler in 1856, consists of mercury (II) iodide ( $\text{HgI}_2$ ) and potassium iodide (KI), which react to form potassium tetraiodomercurate (II) ( $\text{K}_2\text{HgI}_4$ ), in an alkaline solution (KOH or NaOH) [99]. When

added to the low-concentration  $\text{NH}_3$  solution, Nessler's reagent reacts with  $\text{NH}_3$  to form a colored colloidal solution, which can be detected through UV-spectroscopy at wavelength of 420 nm. The detection limit of this method can reach to be 0.02 ppm. It is noteworthy that Nessler's reagent method for ammonia detection is easily interfered by some metal cations ( $\text{Fe}^{3+}$ ,  $\text{Mn}^{2+}$ ,  $\text{Mg}^{2+}$ , etc.), hydrazine, carbonyl compounds, etc. Usually, potassium sodium tartrate tetrahydrate,  $\text{KNaC}_4\text{H}_4\text{O}_6 \cdot 4\text{H}_2\text{O}$  solution is added before Nessler's reagent to eliminate the interference of cations. Then, the indophenol blue method, which can detect the  $\text{NH}_3$  at low concentration of 0.02–1.25 ppm, is based on the Berthelot reaction [100]. In this method, blue colored indophenol is formed after the reaction of  $\text{NH}_3$  with hypochlorite and phenol in the alkaline medium, which can be detected through UV-spectroscopy at wavelength range of 630–650 nm. In this reaction system, sodium nitroprusside ( $\text{Na}_2[\text{Fe}(\text{CN})_5\text{NO}]$ ) is added as catalyst to accelerate the reaction and citrate is also used to prevent the ion precipitation which could be produced in the alkaline condition. The indophenol blue method is sensitive to  $\text{NH}_3$  but is not suitable for detection of high concentrations of  $\text{NH}_3$  because excess  $\text{NH}_3$  could suppress the indophenol blue reaction [101]. Additionally, it is slightly interfered by the organic nitrogen compounds, nitrite, nitrate,  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$  and various electrolytes [102–105]. To avoid using the noxious phenol and producing toxic volatiles during the detection employing indophenol blue method, the salicylate method is developed by replacing phenol with salicylate [106,107]. The color development mechanisms of the two methods are similar but the salicylate method is much safer. Quantitative measurements are usually performed through UV-spectroscopy at the wavelength of 640 nm.

Compared with the colorimetric methods, the IC method is more convenient and efficient for ammonia (especially low-concentration ammonia) detection due to its high sensitivity (detection limit of  $3 \times 10^{-7} \text{ mol L}^{-1}$ ), good reproducibility, high stability and pH compatibility [108,109]. In the instrument, the cations are separated through the columns filled with cation-exchange materials and identified by those characteristic retention times individually. And the quantitative analysis of ammonia is based on the comparison of the obtained peak areas with those of standard samples. Note that, the ions with very close retention times like  $\text{Li}^+$  and  $\text{Na}^+$  could interfere with each other due to the overlap or overlay of peaks [110]. To improve the reliability and accuracy of



Fig. 8. Ammonia quantification techniques assessed with pros (+) and cons (-). Reproduced with permission [93]. Copyright 2020, Elsevier.

ammonia quantification in practical EAS experiments, Yang and co-workers evaluated the accuracy and precision of IC by taking the pH values of electrolyte, the interference  $\text{Li}^+$ ,  $\text{Na}^+$ , 14 kinds of common transition-metal cations ( $5000 \text{ mg L}^{-1}$ ) and 5 kinds of common organic compounds, background and reagents into consideration [111]. According to the analysis results, a rigorous test process is recommended and showed in Fig. 9 to accurately quantify  $\text{NH}_4^+$  by IC method.

The ISE method is sensitive for  $\text{NH}_3$  detection which can show a much larger detection range ( $0.03\text{--}1400 \text{ mg L}^{-1}$ ) [112]. It contains an ammonia ion-sensitive electrode which has a poly(vinylchloride) (PVC) membrane, a reference electrode and voltmeter. Based on the Nernst equation, the potential difference between PVC membrane and the reference electrode depends on the concentration of free ammonium ions in the solution. So, before the measurement, the dissolved ammonia must be completely converted to ammonia ions by adjusting the pH of the tested solution. And, the concentration of ammonium ions in the sample solution is quantified by the standard curve gained from known concentrations of ammonium ions. In the method, some common cations (especially  $\text{K}^+$ ) with high concentrations may affect the measurement accuracy.

Another commonly used quantified method of ammonia is  $^1\text{H}$  NMR spectroscopy which generally combined with  $^{15}\text{N}_2$  isotopic labeling experiments [80,113,114]. The  $^{15}\text{N}_2$  isotopic labeling experiments by replacing  $^{14}\text{N}_2$  with  $^{15}\text{N}_2$  as the feedstock is also employed to verify the origin of the produced  $\text{NH}_3$ . To quantified ammonia concentration, internal standard and external standard methods are generally used. In the internal standard method, maleic acid ( $\text{C}_4\text{H}_4\text{O}_4$ ) with definite concentration is used as the internal standard due to it contains only one chemical shift of H ( $\delta \approx 6.29 \text{ ppm}$ ) and does not interfere the signal peaks of ammonia. And the quantitative analysis of ammonia is based on the comparison of the obtained peak areas with those of maleic acid. As for external standard methods, a series of ammonia solutions with known concentrations are tested and the standard curve related to the

peaks area and concentration is then drew to quantify the sample solution.

Although each of mentioned methods can be able to accurately detect the concentration of ammonia under certain conditions, combining two or more methods is proposed to more reliably and convincingly quantify the ammonia [109,115].

### 3. Structural features and merits of MOF-based electrocatalysts

MOFs are a novel kind of organic-inorganic hybrid crystalline materials with highly ordered porous structure, in which metal cation centers are coordinated with organic ligands to form three-dimensional frameworks [116,117]. To date, more than 20,000 different MOFs have been reported and studied, and it is foreseeable that novel MOFs will continue to be developed in the future [118,119]. Recently, MOF-based materials as electrocatalysts have exhibited distinctive performance because of their unique structural features and merits. Notably, MOFs, usually composed of metal ions and redox-inactive organic ligands, lack free charge carriers and charge transport paths, which show electrical insulator property, resulting in low utilization of active sites of MOFs [120]. To improve the electrical conductivity of pristine MOFs, constructing freestanding MOFs on conductive substrates and intrinsically conductive MOFs, and combining MOFs with conductive materials like nanostructured carbon materials or metal, and conductive polymers to form MOF composites are commonly used methods [120–123]. Additionally, MOFs can be used as templates or precursors to obtain MOF-derived materials (e.g., carbon materials, metal oxides, metal oxides/carbon composites) through thermal treatment, which usually show improved electrical conductivity [119,124–127]. Herein, based on above considerations, we demonstrate structural features and merits of MOF-based electrocatalysts using the classification of pristine MOFs/-MOF composites and MOF derivatives as follows.

#### 3.1. Pristine MOFs/MOF composites

In pristine MOFs/MOF composites, the metal centers generally refer to the metal ions or metal clusters with unoccupied orbitals, and the multidentate organic ligands which contain nitrogen, oxygen, sulfur and so on [128,129]. Benefiting from the diversity of coordination, MOFs/MOF composites own the inherent advantages of highly-developed porosity, tunable composition and structure, so that they have been widely applied in gas adsorption and separation, catalysis, fluorescent sensing and so on [130–134]. The merits and uniqueness of MOFs/MOF composites as the catalytic materials for electrochemical energy conversion can be mainly summarized into the following three aspects:

##### (1) Highly-developed porosity.

Most prominent feature of MOFs is the highly porous structures, which can provide a large area of active interface and evenly dispersed active sites for catalytic reactions. When the MOFs are used as supporting substrate, the abundant pores suggest more hosted sites for active materials and the crystalline frameworks can also further ensure the uniform distribution and efficient immobilization of active materials [135]. In addition to the large active area, the ordered pores show spatial confinement of reactants and provide smooth mass transport channels for the diffusion of electrolyte, which promotes the delivery of reactants and the desorption of products towards and from catalytic sites, thus ensuring the continuous proceedings of the catalytic reaction [136,137]. More attractively, unlike other types of porous materials, the porosity of MOF materials can be predicted or designed through the selection of the metal cations and ligands with specific coordination geometry and connectivity [138].

##### (2) Tunable metal cation centers.

As the core component, metal cations play a central role in determining the structures and functionalities of MOFs [139,140]. The type and amounts of unoccupied orbitals in metal cation influences the

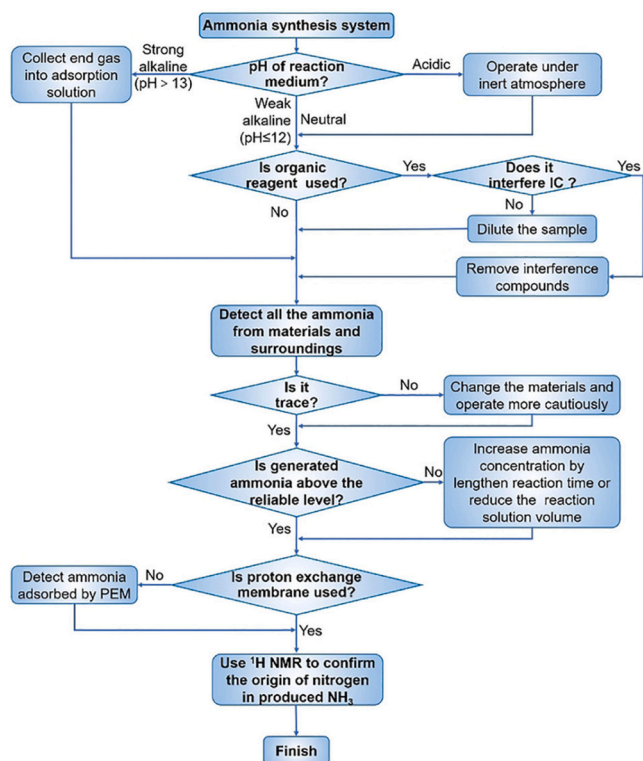


Fig. 9. Flowchart of recommendations that should be considered when performing ammonia synthesis experiments and detecting  $\text{NH}_4^+$  by IC method. Reproduced with permission [111]. Copyright 2019, Wiley-VCH.



spatial arrangement of the coordinated ligands and thus determines the pore shape and size of the porous framework. In this respect, pre-conceived MOFs with specific structure and function can be designed through tuning the metal cation centers. Thanks to the ordered arrangement of metal cations and ligands in MOFs, metal cations are atomically distributed in the framework, which maximizes the utilization of metallic active sites. In addition, when the types and amounts of unoccupied orbitals of two or more metal cations are analogous, multi-metallic centers can be incorporated in the framework and the metal cations are orderly arranged. For the ordered multi-metallic centers, synergistic effects or/and electron interaction may exist in the different active sites, thus improving the catalytic performance. Moreover, the multi-metallic cations can also take effect on the structural modulation. Taking the bimetallic MOF materials as examples, when one of the bimetallic cations acts as the active site, the other can take part in modulating the porous structure.

### (3) Diverse organic ligands.

Organic ligands are the linkers for the distributed metal cations centers through the coordination, which play the role of “skeleton” in MOFs [141]. So diverse selection and design of organic ligands can greatly affect the properties and functions of MOFs. Additionally, organic ligands can also be the source of other non-metallic elements, such as nitrogen, phosphorus and sulfur, which can modify the electronic property of active metal center or directly one-step react with metal cations, partially transition metals, into metal compounds in the MOF derived carton materials [142].

## 3.2. MOF derivatives

Thanks to their characteristic merits, pristine MOFs or their composites have been under intensive studies in electrocatalytic fields. However, they generally face the issues of low stability and electrical conductivity, which greatly hinder the practical application. In this case, by controlled conversion processes like thermal or chemical treatments, MOFs can be converted into their derivatives, including single-metal site catalysts, heteroatom-doped carbon, metal or metal oxide clusters/particles and their complexes, etc., which have a good prospect in the

field of electrocatalytic energy conversion [39,143–146]. Based on the unique advantages of MOFs precursors, MOF derivatives can also inherit the structural features and merits such as controllable hierarchical porous structures with rich and highly dispersed active sites and tunable chemical compositions [147]. Additionally, MOFs can easily be incorporated with various external components such as organic molecules, metal nanoparticles, polyoxometalates and polymers, which can serve as functional components or regulators that induce the formation of targeted and functionalized derivatives [148]. More importantly, MOF derivatives usually show improved electrical conductivity benefited from the carbon formation and enhanced stability for electrocatalysis because no breaks of coordination bonds occur in the derivatives [149]. And both metallic and non-metallic elements can participate in the formation of MOF derivatives, which may act as active sites for electrocatalysis [150]. Lastly, the low-cost and simple synthesis process offers potential large-scale production routes of MOF derivatives for eventual industrial applications.

## 4. MOF-based electrocatalysts for EAS from various nitrogen sources

Based on above discussions, using the classification of MOF-based electrocatalysts including pristine MOFs/MOF composites and MOF derivatives, we summarize recent progress of  $\text{NH}_3$  synthesis via ERRs from various nitrogen sources under ambient conditions in this section. More intuitively, the advanced pristine MOFs/MOF composites and MOF derivatives as electrocatalysts for EAS from various nitrogen sources are listed in Table 1 and Table 2, respectively.

### 4.1. Pristine MOFs/MOF Composites

#### 4.1.1. NRR

Tunable chemical environments of the pores or channels and periodical arranged metal sites of MOFs make they have great potential to concentrate and activate  $\text{N}_2$ , thus they have attracted great interest to serve as electrocatalysts for ammonia synthesis from  $\text{N}_2$  reduction [45, 174,175]. In 2017, Zhao and co-workers first reported the application of

**Table 1**  
Summary of pristine MOFs/MOF composites as electrocatalysts for EAS from various nitrogen sources.

Nsource	Catalyst	Electrolyte	$\text{NH}_3$ Yield	FE	Detection method	Ref.
$\text{N}_2$	PCN-222(Fe)	0.1 M HCl	110.9 $\mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$	70.7%	Nessler's reagent	[45]
	In-MOF	0.05 M $\text{H}_2\text{SO}_4$ /0.01 M KOH	24.70 $\mu\text{g h}^{-1} \text{mg}^{-1}$ 79.20 $\mu\text{g h}^{-1} \text{mg}^{-1}$	6.72% 14.98%	Indophenol blue	[151]
	NiFe-MOF	0.1 M $\text{NaHCO}_3$	9.3 $\mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$	11.5%	Indophenol blue	[152]
	HT Au@MOF	0.1 M $\text{Na}_2\text{SO}_4$	49.5 $\mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$	60.9%	Nessler's reagent	[153]
	60 nm Pt/Au@ZIF	$\text{LiCF}_3\text{SO}_3$ (0.2 M) in ethanol (1%)/THF	161 $\mu\text{g mg}_{\text{cat}}^{-1} \text{h}^{-1}$	44%	Indophenol blue	[154]
	Ag-Au@ZIF	$\text{LiCF}_3\text{SO}_3$ (0.2 M) in ethanol (1%)/THF	10 $\mu\text{mol cm}^{-2} \text{s}^{-1}$	18%	Indophenol blue	[155]
	ZIF-67 @ $\text{Ti}_3\text{C}_2$	0.1 M KOH	6.52 $\mu\text{mol h}^{-1} \text{cm}^{-2}$	20.2%	Indophenol blue	[156]
	$\text{MoS}_2$ @ZIF-71	$\text{Na}_2\text{SO}_4$	56.69 $\mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$	30.91%	Indophenol blue	[157]
	NCNT@MIL-101(Fe)	0.05 M $\text{H}_2\text{SO}_4$	6.97 $\mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$	25.15%	Indophenol blue	[158]
	MIL-101(Fe)/ $\text{MoS}_3$	0.1 M HCl	25.7 $\mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$	36.71%	Indophenol blue	[159]
	PdCu@UiO-S@PDMS	0.1 M HCl	20.24 $\mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$	13.16%	Indophenol blue	[160]
	$\text{Co}_3\text{Fe-MOF}$	0.1 M KOH	8.79 $\mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$	25.64%	IC	[161]
	UiO-66- $\text{NH}_2$	0.1 M $\text{Na}_2\text{SO}_4$	52.81 $\mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$	85.21%	Indophenol blue	[162]
	Pd-TA	0.1 M $\text{Na}_2\text{SO}_4$	24.12 $\mu\text{g h}^{-1} \text{cm}^{-2}$	9.49%	Indophenol blue	[163]
	NPG@ZIF-8	0.1 M $\text{Na}_2\text{SO}_4$	28.7 $\mu\text{g h}^{-1} \text{cm}^{-2}$	44%	Indophenol blue	[54]
	Fe-TCPP	0.1 M HCl	44.77 $\mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$	16.23%	Indophenol blue	[164]
	Cu@Ce-MOF	0.1 M KOH	14.83 $\mu\text{g h}^{-1} \text{cm}^{-2}$	10.81%	Indophenol blue	[165]
	MIL-100 (Al)	0.1 M KOH	10.6 $\mu\text{g h}^{-1} \text{cm}^{-2} \text{mg}_{\text{cat}}^{-1}$	22.6%	Indophenol blue	[166]
	Cu@CuHHTP	0.5 M $\text{Na}_2\text{SO}_4$ + 500 ppm $\text{NO}_3^-$	1.84 $\text{mg h}^{-1} \text{cm}^{-2}$	67.55%	Indophenol blue	[167]
	NiCoBDC@HsGDY	1.0 M KOH + 0.1 M $\text{NO}_3^-$ 0.5 M $\text{Na}_2\text{SO}_4$ + 0.1 M $\text{NO}_3^-$	0.56 $\text{mmol h}^{-1} \text{cm}^{-2}$ 0.39 $\text{mmol h}^{-1} \text{cm}^{-2}$	99.1% 99.7%	Nessler's reagent	[168]
$\text{NO}_3^-/\text{NO}_2^-$	$\text{Cu}_3(\text{BTC})_2$ @HsGDY	0.5 M $\text{Na}_2\text{SO}_4$ + 200 ppm $\text{KNO}_3$	0.24 $\text{mmol h}^{-1} \text{cm}^{-2}$	90.2%	Nessler's reagent	[169]
	Pd-NDs/Zr-MOF	0.1 M $\text{Na}_2\text{SO}_4$ + 500 ppm $\text{NO}_3^-$	287.31 $\text{mmol h}^{-1} \text{g}_{\text{cat}}^{-1}$	58.1%	Indophenol blue	[170]
	$\text{Ru}_x\text{O}_y/\text{RuNi-MOF}$	0.1 M $\text{Na}_2\text{SO}_4$ + 50 ppm $\text{NO}_3^-$ -N	274 $\mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$	72.56%	Nessler reagent	[171]
	$\text{Fe}_2\text{Co-MOF}$	0.05 M $\text{H}_2\text{SO}_4$ + 50 g $\text{L}^{-1}$ $\text{KNO}_3$	3463.3 $\mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$	90.55%	Indophenol blue	[172]
	UiO-CuZn	0.5 M $\text{Na}_2\text{SO}_4$ + 200 ppm $\text{NO}_3^-$	0.22805 $\text{mmol g}^{-1} \text{h}^{-1}$	91.4%	Indophenol blue	[173]



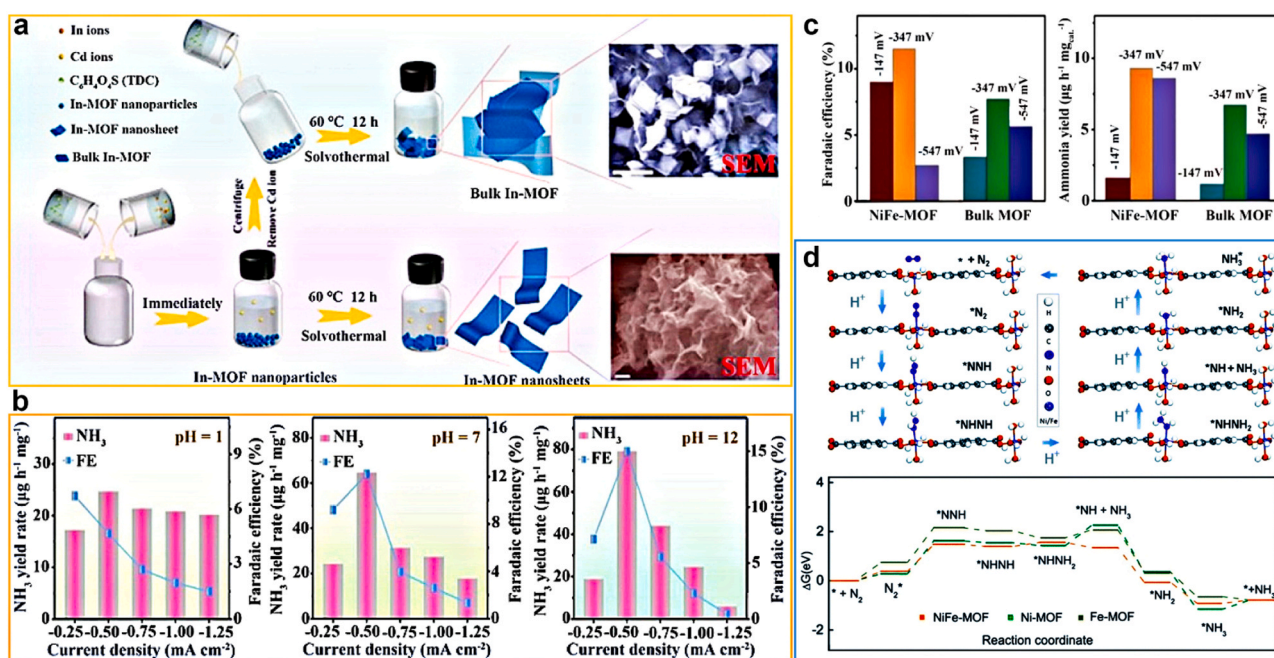
**Table 2**

Summary of MOF derivatives as electrocatalysts for EAS from various nitrogen sources.

N source	Catalyst	Electrolyte	NH <sub>3</sub> Yield	FE	Detection method	Ref.
N <sub>2</sub>	S/N-MPC	0.05 M H <sub>2</sub> SO <sub>4</sub>	45.51 $\mu\text{g}_{\text{NH}_3} \text{mg}_{\text{cat}}^{-1} \text{h}^{-1}$	25.16%	Indophenol blue	[185]
	Co@NC	0.1 M Na <sub>2</sub> SO <sub>4</sub>	$1.58 \times 10^{-10} \text{ mol s}^{-1} \text{ cm}^{-2}$	21.79%	Indophenol blue	[186]
	NC@Ru-5	0.1 M KOH	16.68 $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	14.23%	Nessler's reagent	[187]
	Fe <sub>2</sub> O <sub>3</sub> @-MoS <sub>2</sub>	0.1 M Na <sub>2</sub> SO <sub>4</sub>	112.15 $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	8.62%	Indophenol blue	[188]
	CoRu@NC	0.1 M KOH	56.82 $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	2.02%	Nessler's reagent	[189]
	TiO <sub>2</sub> /CeO <sub>2</sub>	0.1 M HCl	8.8 $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	22.3%	Indophenol blue	[190]
	Ru SAs/N-C	0.05 M H <sub>2</sub> SO <sub>4</sub>	120.9 $\mu\text{g}_{\text{NH}_3} \text{mg}_{\text{cat}}^{-1} \text{h}^{-1}$	29.6%	Indophenol blue	[191]
	Fe <sub>1</sub> -N-C	0.1 M HCl	$1.56 \times 10^{-11} \text{ mol cm}^{-2} \text{ s}^{-1}$	4.51%	Indophenol blue	[192]
	Mo-SA/PNC	0.05 M H <sub>2</sub> SO <sub>4</sub>	15.34 $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	24.03%	Indophenol blue	[180]
	MoFe-PC	0.1 M HCl	34.23 $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	16.83%	Indophenol blue	[193]
	Mo-Co/NC	0.1 M Na <sub>2</sub> SO <sub>4</sub>	89.8 $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	13.5%	Indophenol blue	[194]
	C-Ti <sub>x</sub> O <sub>y</sub> /C	0.1 M LiClO <sub>4</sub>	14.8 $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	17.8%	Indophenol blue	[195]
	CoP HNC	1.0 M KOH	10.78 $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	7.36%	Indophenol blue	[196]
	C@YSZ	0.1 M Na <sub>2</sub> SO <sub>4</sub>	24.6 $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	8.2%	Nessler's reagent	[197]
	ISAS-Fe/NC	0.1 M PBS	62.9 $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	18.6%	Indophenol blue	[198]
	MoP@PPC	0.1 M HCl	28.73 $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	2.48%	Indophenol blue	[199]
	Co@NC	0.1 M NaOH+ 0.1 M NO <sub>3</sub> <sup>-</sup>	758 $\mu\text{mol h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	96.5%	Indophenol blue	[200]
	Cu@C	1.0 M KOH+ 1 mM NO <sub>3</sub> <sup>-</sup>	469.5 $\mu\text{g h}^{-1} \text{ cm}^{-2}$	72%	Indophenol blue	[201]
	Cu(I)-N <sub>3</sub> C <sub>1</sub> SAC	50 mM Na <sub>2</sub> SO <sub>4</sub> + 100 ppm NO <sub>3</sub> <sup>-</sup> -N	50.3 $\mu\text{mol mg}_{\text{cat}}^{-1} \text{ h}^{-1}$	65.3%	Nessler's reagent	[202]
NO <sub>3</sub> <sup>-</sup> / NO <sub>2</sub> <sup>-</sup>	Cu/Pd/CuOx	0.5 M K <sub>2</sub> SO <sub>4</sub> + 50 mg L <sup>-1</sup> NO <sub>3</sub> <sup>-</sup> -N	1510 $\mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$	84.04%	Nessler's reagent	[203]
	Ru <sub>15</sub> Co <sub>85</sub>	0.1 M KOH+ 0.1 M KNO <sub>3</sub>	3.21 $\text{mol g}_{\text{cat}}^{-1} \text{ h}^{-1}$	96.78%	salicylate <sup>1</sup> H NMR	[204]
	CuNi/NC	0.1 M PBS+ 50 mg L <sup>-1</sup> NO <sub>3</sub> <sup>-</sup> -N	n/a	79.6%	Gas-phase molecular absorption spectrograph	[205]
	Ru SA-NC	1.0 M KOH+ 0.5 M NO <sub>3</sub> <sup>-</sup> 1.0 M KOH+ 0.5 M NO <sub>2</sub> <sup>-</sup>	0.11 $\text{mmol h}^{-1} \text{ cm}^{-2}$ 0.69 $\text{mmol h}^{-1} \text{ cm}^{-2}$	72.8% 97.8%	Indophenol blue	[206]
	Cu-N-C	1.0 M KOH+ 1.0 M KNO <sub>3</sub>	13.8 $\text{mol}_{\text{NH}_3} \text{g}_{\text{cat}}^{-1} \text{ h}^{-1}$	95.5%	Nessler's reagent	[207]
	Cu/Ni-NC	0.5 M Na <sub>2</sub> SO <sub>4</sub> + 100 ppm NO <sub>3</sub> <sup>-</sup> -N	5480 $\text{mg h}^{-1} \text{ mg}_{\text{cat}}^{-1} \text{ cm}^{-2}$	97.28%	Nessler's reagent	[208]
	MR Co-NC	0.1 M KOH+ 0.1 M KNO <sub>3</sub>	1.25 $\text{mmol h}^{-1} \text{ cm}^{-2}$	95.35%	IC	[209]
	Co-NPs	0.1 M PBS+NO	244 $\mu\text{mol mg}_{\text{cat}}^{-1} \text{ h}^{-1}$	92.3%	H NMR	[210]

MOFs as NRR electrocatalysts at low temperature and ambient pressure [176]. A series of MOFs (M) (M = Fe, Co, Cu) were synthesized in this work, among which the Fe-based MOF displayed the best catalytic activity: NH<sub>3</sub> yield and a low faradaic efficiency (FE) value are  $2.12 \times 10^{-9} \text{ mol s}^{-1} \text{ cm}^{-2}$  and 1.43%, respectively, at 1.2 V and 90 °C using pure N<sub>2</sub> and water as raw materials. According to their results, porous MOFs can offer massive metal sites with empty d-orbitals, which served as N<sub>2</sub>

adsorbent and Lewis acid to adsorb and activate N<sub>2</sub> molecules on the electrode surface. Afterwards, more monometallic MOFs, such as Fe, Co, Zn, Cu, Al, Zr, Ce, and In, have been explored for NH<sub>3</sub> synthesis via NRR. Typically, Zhang et al. developed well-defined single-site MOFs (M-TCPP; M = Fe, Co, or Zn) as electrocatalysts for electrocatalytic N<sub>2</sub> reduction. The prepared Fe-TCPP showed outstanding performance with high NH<sub>3</sub> yield of  $44.77 \mu\text{g h}^{-1} \text{ mg}_{\text{cat}}^{-1}$  and FE of 16.23%, superior to



**Fig. 10.** (a) The synthesis and morphological characterization of In-MOF nanosheets. (b) NRR performances of In-MOFs in different pH electrolytes. (c) FEs and NH<sub>3</sub> yields of NiFe-MOF and bulk MOF at different potentials, (d) Density functional theory calculations of NiFe-MOF and its counterparts. Reproduced with permission [151]. Copyright 2021, Royal Society of Chemistry. Reproduced with permission [152]. Copyright 2020, Royal Society of Chemistry.

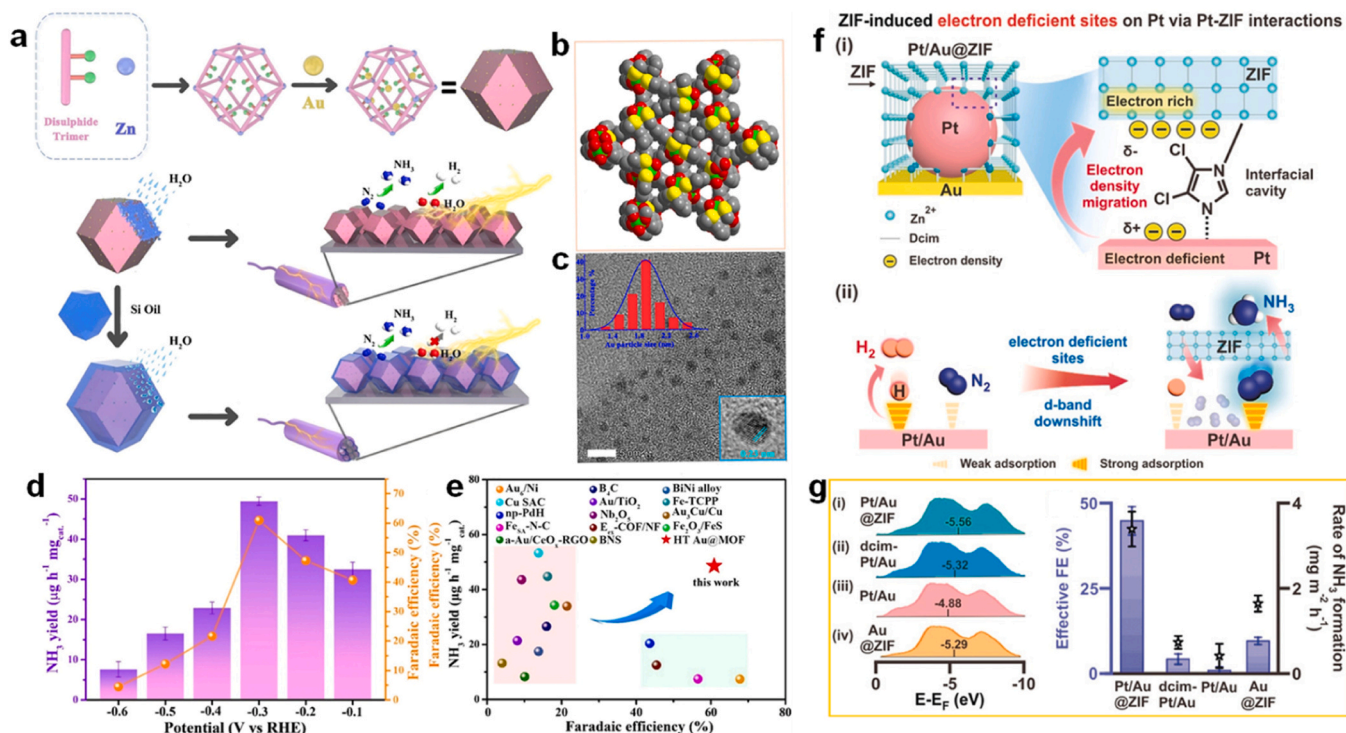
those of most reported MOF catalysts. This work expounded the single Fe site promoted the formation of the key  $^*NNH$  intermediate during the hydrogenation of  $N_2$ . Although pristine MOF materials as NRR electrocatalysts show potential applications, the poor conductivity is a tough obstacle in electrocatalytic applications. In this regard, conductive two-dimensional (2D) MOF nanosheets are considered more attractive candidates based on some theoretical predicts [177,178]. Duan and co-authors prepared 2D In-MOFs nanosheets with a thickness of 1.3 nm via an ion exchange and dissolution-recrystallization mechanism (Fig. 10a) [151]. Benefited from the high porosity and excellent electrical conductivity, the 2D In-MOFs exhibited excellent electrocatalytic NRR performance in a full pH range: The maximum  $NH_3$  yields of 24.70, 64.73, and  $79.20 \mu g h^{-1} mg^{-1}$  at different the pH value of 1, 7, and 12, respectively (Fig. 10b). Except for the improvement of the conductivity, incorporating second or third metal ions into the MOF materials is a good strategy to adjusting the center value of d-band of metals to enhance their catalytic performance. For example, Zhao group reported bimetallic NiFe-MOF NPs with an average particle size of  $5.5 \pm 1.8$  nm as electrocatalyst for NRR. The NiFe-MOF nanodots showed the excellent catalytic activity of  $NH_3$  yield ( $9.3 \mu g h^{-1} mg_{cat}^{-1}$ ) and FE (11.5%) at  $-0.374$  V versus RHE at ambient temperature (Fig. 10c) [152]. Mechanistic investigations reveal that the better NRR activity of bimetallic MOFs than that of the corresponding monometallic materials is attributed to the synergy of both Fe and Ni cations in the bimetallic system. And theoretical research highlights the iron doping effect can suppress the energy barrier of the first ammonia release step (Fig. 10d).

Based on the rich well-defined porosity, MOFs possess large surface areas, which can also be implemented as host for high-active metal nanoparticles. The active metal nanoparticles are confined in the channels, which can effectively inhibit the aggregation of the particles during the catalytic process. Meanwhile, the hydrophobicity of MOF matrices can efficiently suppress the mass transfer of  $H_2O$  and further weaken the competitive HER during the aqueous electrocatalytic  $N_2$

reduction. For example, Du and co-authors developed a porous three-dimensional (3D) Zn-based MOF with high porosity and rich disulfide bonds to confine Au NPs with ultrafine size of  $1.9 \pm 0.4$  nm through integration of dynamic covalent chemistry and coordination chemistry [153]. Subsequently, Au@MOF was modified with organosilicon to enhance the hydrophobicity, which can strongly inhibit the competitive HER (Fig. 11a). The active Au particles were confined in the caged-shaped Zn-based MOFs (Fig. 11b, c). Consequently, the hydrophobic Au@MOF composite shows excellent electrocatalytic NRR performances: the highest  $NH_3$  yield of  $49.5 \mu g h^{-1} mg_{cat}^{-1}$  and FE of 60.9% at  $-0.3$  V versus RHE in  $0.1$  M  $Na_2SO_4$ , surpassing most MOF based catalysts (Fig. 11d, e). Additionally, Ling's group reported polycrystalline zeolitic imidazolate frameworks (ZIF) layer on the Pt nanosphere-deposited Au electrode [154]. The ZIF layer played three main roles: 1) stimulating the electron-deficient catalytic sites to regulate the d-band of Pt/Au, 2) act as a hydrophobic layer to block the water, 3) enhancing the adsorption  $N_2$  molecules. The designed Pt/Au@ZIF achieved a high  $NH_3$  yield of  $> 161 \mu g h^{-1} mg_{cat}^{-1}$  and FE of  $> 44\%$  at ambient conditions, being superior to other Au-Pt electrocatalysts without ZIF (Fig. 11f, g). Recently, other MOF-based composites, such as PdCu@UiO-S@PDMS [160], Au/ZrO<sub>2</sub> [179], Mo-based ZIF-8 derivatives [180], Ag-Au@ZIF [155], ZIF-67@Ti<sub>3</sub>C<sub>2</sub> [181], MoS<sub>2</sub>@ZIF-71 [157], CNT/NCNT@UiO-66 [158], MIL-101(Fe)/MoS<sub>3</sub> [159], Pd/HKUST-1 [182] have also been developed for electrocatalytic NRR. In general, incorporating MOFs into other active materials will blend the benefits of each other, thereby showing great potentials for efficiently electrocatalytic  $N_2$ -to- $NH_3$ .

#### 4.1.2. $NO_3^-$ RR/ $NO_2^-$ RR

Conductive MOF materials, with dispersed planar metal nodes and unique  $\pi$ -conjugated structures, are promising encapsulates to confine small metal species and protect metal species from aggregation [183]. Lu et al. first developed the conductive copper-based MOF (CuHHTP,



**Fig. 11.** (a) Schematic depicting a hydrophobic Au@MOF for the electrocatalytic NRR, (b) The 3D crystal structure of Au@MOF, (c) TEM images of Au@MOF with the size distribution of Au NPs, (d)  $NH_3$  yield and FE at different potentials, (e) A comparison of NRR performances of  $NH_3$  yield and FE for HT Au@MOF with other reported materials. (f) Schematic illustration of the function of ZIF, (g) Evaluation of d-band position and corresponding effective FE and rate of ammonia formation for each system, respectively.

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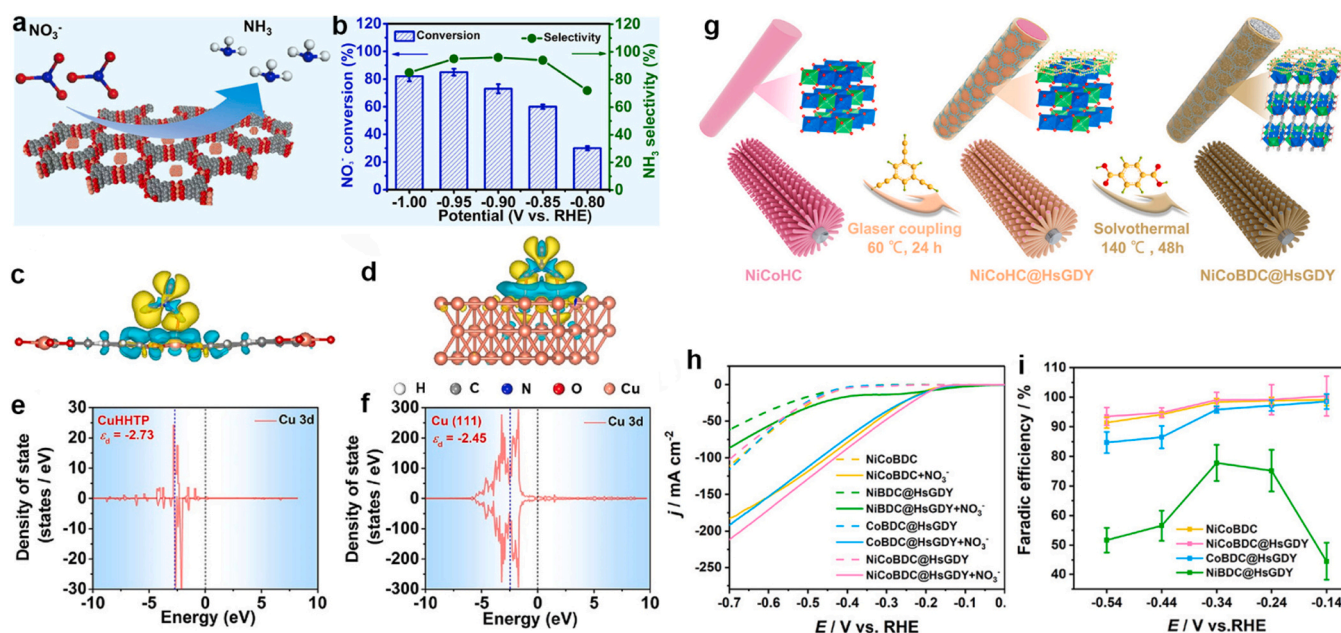
HHTP = 2,3,6,7,10,11-hexahydroxytriphenylene) nanorods for electrocatalytic nitrate reduction [167]. During the electrochemical  $\text{NO}_3^-$  reduction process, the CuHHTP nanorods were in situ reduced into metallic Cu clusters confined in the CuHHTP (Cu@CuHHTP, Fig. 12a). The in situ generated Cu@CuHHTP exhibited superb performance for nitrate electroreduction: a high  $\text{NO}_3^-$  conversion of 85.81% and 96.84% selectivity for  $\text{NH}_3$  (Fig. 12b). From the density functional theory (DFT) calculations results, there is  $0.57\text{ e}^-$  transferred from CuHHTP to  $\text{NO}_3^-$  species, which less than that on Cu (111) ( $0.70\text{ e}^-$ , Fig. 12c, d), indicating the stronger interaction between Cu(111) and  $\text{NO}_3^-$ . Additionally, the 3d orbit of Cu can not only obtain electrons but also lose electrons, and this “accept–donate” mechanism is more favorable for the adsorption of reaction intermediates. Both the higher  $\epsilon_d$  and the “accept–donate” mechanism in charge transfer for Cu(111) ensure the high performance of Cu@CuHHTP (Fig. 12e, f). Considering that EAS from nitrate is highly dependent on the coupling reaction of nitrate and water, interfacial engineering is anticipated to promote the deoxygenation and hydrogenation of nitrate with water. Zhuo et al. developed the hybrid NiCoBDC@HsGDY nanoarray by engineering the surface of bimetallic Ni/Co-MOFs (NiCoBDC) with hydrogen-substituted graphdiyne (HsGDY) for promoting EAS performance [168]. The preparation process of NiCoBDC@HsGDY nanowire array was displayed in Fig. 12g. The decoration of HsGDY on the surface of NiCoBDC facilitates both electrons and  $\text{NO}_3^-$  ions gathering between NiCoBDC and HsGDY, thus converting rate-determining step and further promoting the efficiency of EAS (Fig. 12h, i). Similarly, they also explored a suite of Cu-MOF hybrid nanoarrays encapsulated with HsGDY tubular shells as effective electrocatalysts for selective nitrate-to-ammonia conversion and achieved good result [169]. Additionally, most state-of-the-art electrocatalysts achieved high  $\text{NO}_3^-$ RR efficiencies in neutral or alkaline electrolytes, while Ding and coworkers successfully developed a series of  $\text{Fe}_2\text{M}$  ( $\text{M} = \text{Fe}, \text{Co}, \text{Ni}, \text{Zn}$ ) trinuclear cluster MOFs that enable the highly efficient electrocatalytic  $\text{NO}_3^-$ RR to  $\text{NH}_4^+$  under strong acidic conditions [172]. Fig. 13a showed 3D framework of  $\text{Fe}_2\text{M}$ -MOF with different trinuclear metal clusters and the tetrakis(1,1'-biphenyl-4-carboxylic acid)-1,4-benzenediamine ( $\text{H}_4\text{TPBD}$ ) ligand, in which each  $\text{H}_4\text{TPBD}$  ligand is linked to four  $\text{Fe}_2\text{M}$  clusters. Electrochemical  $\text{NO}_3^-$ RR performance of

different  $\text{Fe}_2\text{M}$ -MOFs was systematically evaluated in  $0.05\text{ M H}_2\text{SO}_4$  ( $\text{pH} = 1$ ) with  $50\text{ g L}^{-1}\text{ KNO}_3$  electrolytes. From the linear sweep voltammetry (LSV) curves (Fig. 13b), we can see the  $\text{NO}_3^-$ RR activities of  $\text{Fe}_2\text{M}$ -MOFs can be summarized as  $\text{Co} > \text{Fe} > \text{Ni} > \text{Zn}$ . And  $\text{Fe}_2\text{Co}$ -MOFs also showed the best average  $\text{NH}_3$  yield rates and the corresponding FEs- $\text{NH}_3$  in the range of  $15\text{--}100\text{ g L}^{-1}\text{ KNO}_3$  (Fig. 13c). DFT computations results indicated that the best performance of  $\text{Fe}_2\text{Co}$ -MOFs could be attributed to the lowering the energy consumption of the  $\text{NO}_3^-$  adsorption and NO hydrogenation steps (Fig. 13d). And during the electrochemical process, two quasi-reversible single-electron processes were observed in  $\text{Fe}_2\text{Co-N}_2\text{-MOF}$  (with  $\text{H}_4\text{TPBD}$  ligand), which can be attributed to  $\text{N/N}^+/\text{N}^{2+}$  redox couples (Fig. 13e). This pioneering work provides new insights into the design principles of high-performance  $\text{NO}_3^-$ RR catalysts under strong acidic conditions.

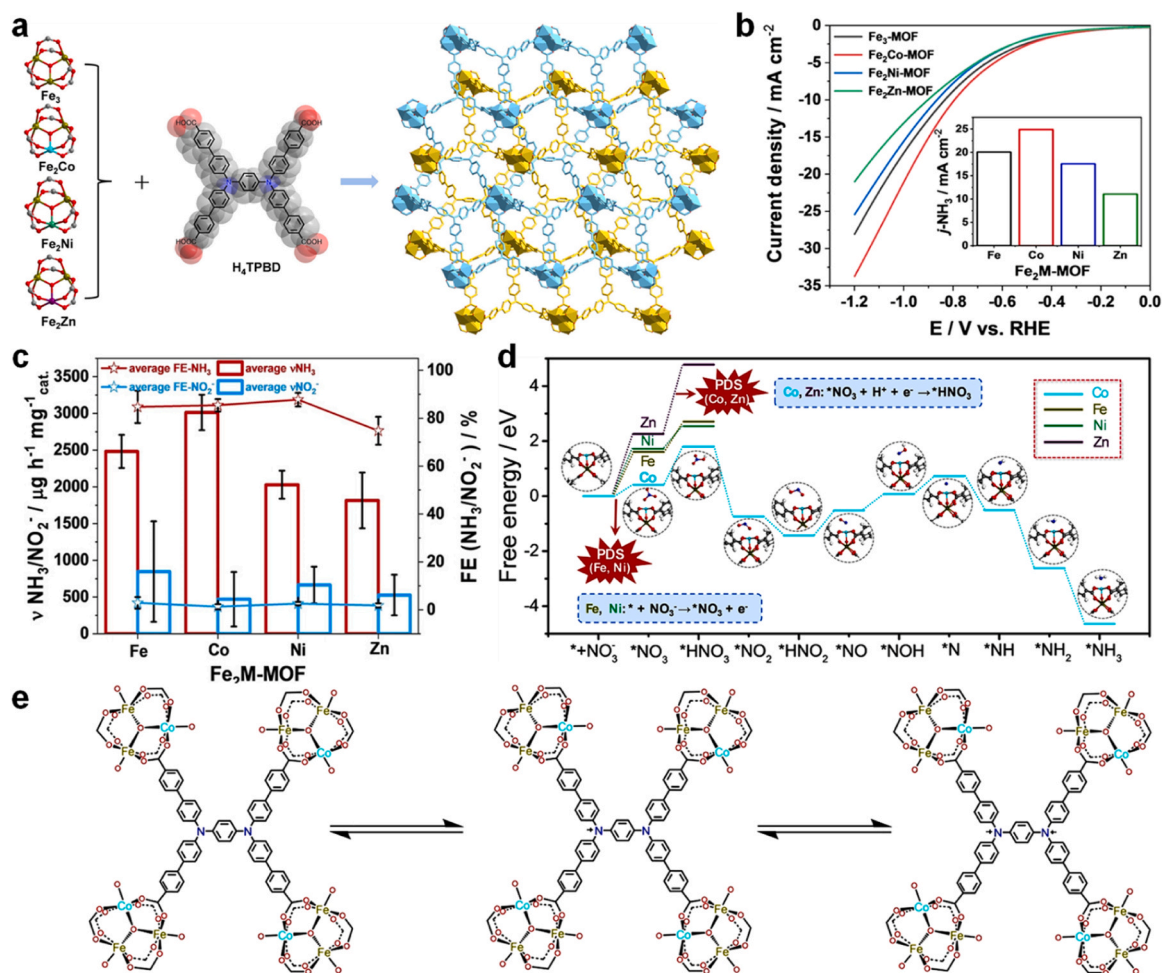
Benefited from the high specific surface area, the conductive MOF materials also were applied as the support materials for the post-prepared active materials for electrochemical nitrate reduction to ammonia. For example, Jin and colleagues load the uniform noble metal nanodots (M-NDs,  $\text{M} = \text{Pb}, \text{Ag}, \text{Au}$ ) on the stable and conductive Zr-MOF [170]. The good conductivity of Zr-MOF can facilitate the mass transfer process. Among M-NDs/Zr-MOF materials, Pd-NDs/Zr-MOF exhibited the best activity with a  $\text{NH}_3$  yield of  $287.31\text{ mmol h}^{-1}\text{ g}^{-1}$  and a FE of 58.1% (Fig. 14a, b). In addition, Ye and coworkers reported  $\text{Ru}_x\text{O}_y$  clusters stabilized on RuNi-MOFs for ammonia synthesis from nitrate [171]. Fig. 14c is the preparation process, and the RuNi-MOFs exhibited nearly 100%  $\text{NH}_4^+$  selectivity (Fig. 14d). From these works, it can be found that MOFs may be a good supporter for active catalysts benefited the dispersion, stabilization and synergistic effect.

#### 4.1.3. NORR

Benefitted from the porous structures, MOFs are expected to act as efficient electrocatalysts for gaseous  $\text{NO}_x$  pollutant to  $\text{NH}_3$ . Although no experimental study of MOF materials for  $\text{NO}_x$  reduction have been reported, Li et al. conducted the DFT calculations of A 2D MOF with hexaaminobenzene (HAB) ligands (TM-HAB MOF, TM = Ti, V, Cr, Mn, Fe, Co, Ni, Cu, Mo, Ru, Rh and Pd) as an electrocatalyst for electrochemical NO to  $\text{NH}_3$  [184]. Among the mentioned metal-based MOF



**Fig. 12.** (a) Schematic diagram of Cu@CuHHTP for  $\text{NO}_3^-$ RR, (b)  $\text{NO}_3^-$  conversion and  $\text{NH}_3$  selectivity over Cu@CuHHTP, Charge density difference of  $\text{NO}_3^-$  adsorption on (c) CuHHTP and (d) Cu(111), Density of states for (e) CuHHTP and (f) Cu(111), (g) Schematic illustration for the preparation of NiCoBDC@HsGDY nanowire array, (h) LSV curves of different samples in 1 M KOH with and without 0.1 M  $\text{NO}_3^-$ , (i) Potential-dependent FEs of different samples. Reproduced with permission [167]. Copyright 2022, American Chemical Society. Reproduced with permission [168]. Copyright 2023, American Chemical Society.



**Fig. 13.** (a) 3D framework of Fe<sub>2</sub>M-MOF with different trinuclear metal clusters and the H<sub>4</sub>TPBD ligand, (b) LSV curves of Fe<sub>2</sub>M-MOFs in 0.05 M H<sub>2</sub>SO<sub>4</sub> (pH = 1) with 50 g L<sup>-1</sup> KNO<sub>3</sub> electrolyte (inset depicts the partial current densities of ammonia production at -1.1 V<sub>RHE</sub>), (c) The average NH<sub>3</sub> yield rates and the corresponding FE-NH<sub>3</sub> of Fe<sub>2</sub>M-MOFs at -1.1 V<sub>RHE</sub> in 0.05 M H<sub>2</sub>SO<sub>4</sub> electrolyte (pH = 1) with the range of 15–100 g L<sup>-1</sup> KNO<sub>3</sub>, (d) Free energy diagram and PDS of electrochemical conversion from NO<sub>3</sub><sup>-</sup> to NH<sub>3</sub> in Fe<sub>3</sub>, Fe<sub>2</sub>Co, Fe<sub>2</sub>Ni, and Fe<sub>2</sub>Zn systems, (e) Schematic diagram of the different redox states of the nitrogen containing H<sub>4</sub>TPBD ligand, where the nitrogen atoms promote both the redox transition (electron transfer) and protonation within the Fe<sub>2</sub>Co-N<sub>2</sub>-MOF structure. Reproduced with permission [172]. Copyright 2023, Wiley-VCH.

materials, the suitable candidates are Co- and Rh-HAB MOFs due to moderate binding strength between NO and substrates (Fig. 15a, b). Fig. 15c, d show all intermediates of electrochemical NO reduction catalyzed by Co-HAB and Rh-HAB monolayers, and the optimal reaction pathway, respectively. From the theoretical analysis, it can be found that the hydrogenation of NO for ammonia synthesis is feasible at low NO coverage, especially for Co-HAB MOF with low potential and high selectivity. These theoretical results offer the scientific guidance for the design and development of high-efficiency catalysts for electrochemical NO to ammonia.

#### 4.2. MOF derivatives

In view of the depressed conductivity and stability of most MOFs, high-temperature carbonization of MOFs to synthesize MOF derivatives, such as heteroatom-doped porous carbon-based materials, metal/metal compounds and single-metal-atom catalysts, has caught more attention for developing excellent electrocatalysts for EAS via ERRs from various nitrogen sources.

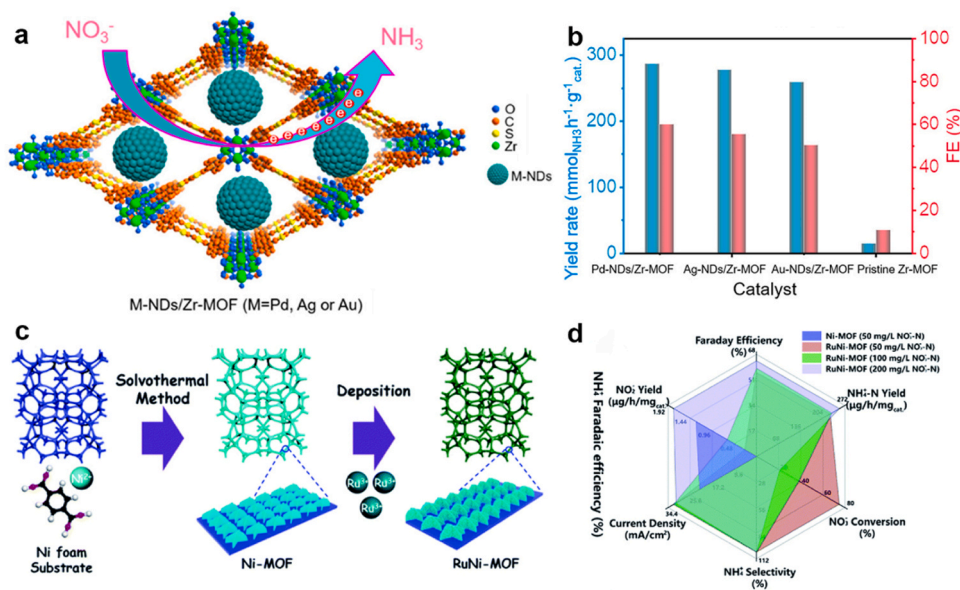
##### 4.2.1. NRR

Heteroatom in porous carbon can not only increase the active sites but also introduce carbon defects and charge polarization of the carbon

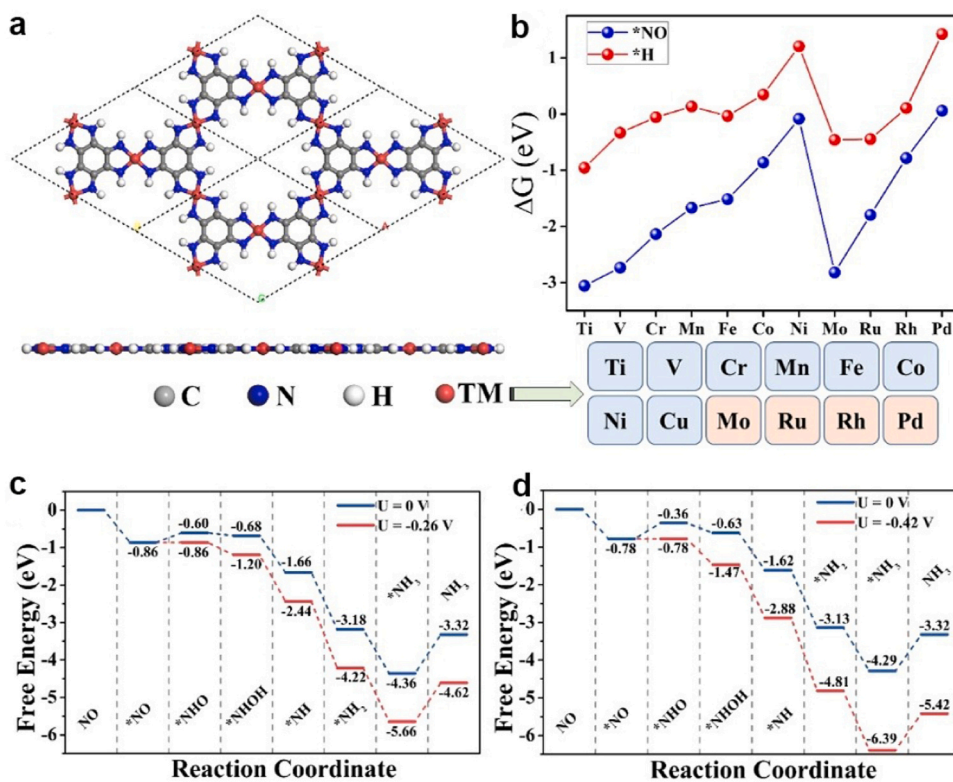
material, thereby facilitating nitrogen activation. Zhao and coworkers reported N-doped porous carbon (NPC) catalysts synthesized via pyrolysis of ZIF-8 at 750 °C (NPC-750), 850 °C (NPC-850), 950 °C (NPC-950) for electrocatalytic NRR (Fig. 16a) [211]. From both theoretical and experimental tests, the NPC-750 possessed the highest pyridinic and pyrrolic N content of 13.6 at% compared with NPC-850 (5.5 at%) and NPC-950 (2.1 at%), which can promote producing carbon defects and be the active sites for N<sub>2</sub> molecule adsorption and activation. So, the NRR catalytic property of NPC-750 was distinctly better than those of NPC-850 and NPC-950 at -0.7 and -0.9 V vs. RHE (Fig. 16b, c). Except for the NPC, N, P co-doping carbon [212], S/NMPC [185] derived from MOFs have also been explored for NRR.

Reasoned from core component of the metal center, MOFs can be converted into metals and metal oxide/phosphide/chalcogenide via the pyrolysis process, which also possess high porosity and plenty of active sites. And the feasibility of introducing multiple metals into MOF materials as precursors can increase the number of active sites or the synergistic effect for electrocatalytic applications. So, MOF-derived metal/metal compounds have caught much attention as efficient electrocatalysts for NRR. In 2019, metallic Co encapsulated in N doped carbon (Co@NC), which was derived from ZIF-67, was synthesized by Yin's group [186]. The Co@NC acted as electrocatalyst for NRR achieved an excellent performance (NH<sub>3</sub> yield of 1.57 × 10<sup>-10</sup> mol s<sup>-1</sup> cm<sup>-2</sup>





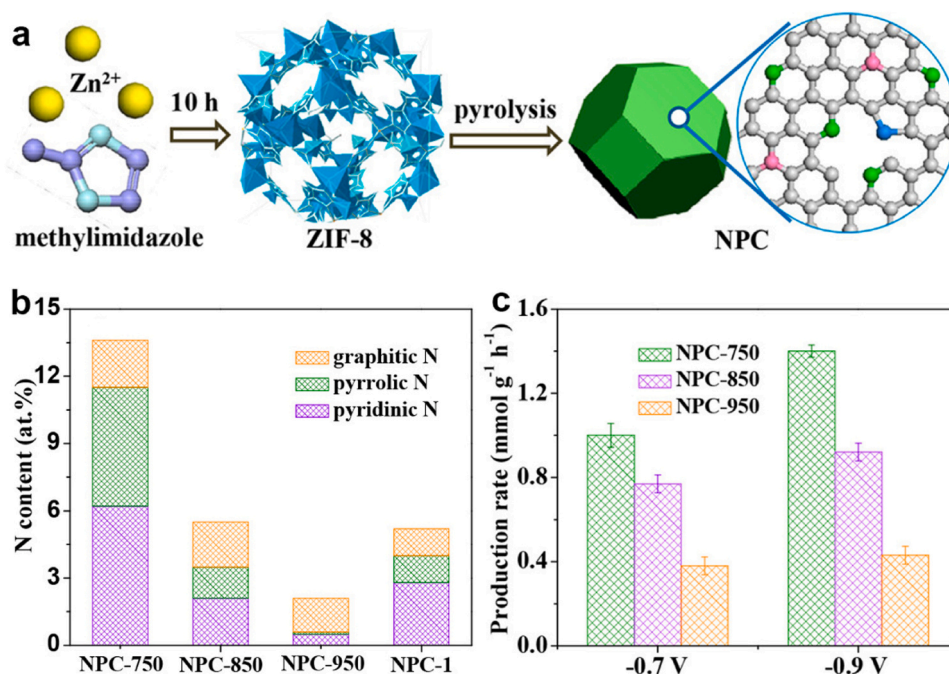
**Fig. 14.** (a) Schematic diagram of M-NDs/Zr-MOF for  $\text{NO}_3\text{RR}$ , (b) Comparison of the  $\text{NH}_3$  yields and FE values of different catalysts at  $-1.3$  V vs. RHE, (c) Schematic illustration of the preparation of the RuNi-MOF catalyst, (d) Comparison of the catalytic performances between the Ni-MOF and RuNi-MOF. Reproduced with permission [170]. Copyright 2022, American Chemical Society. Reproduced with permission [171]. Copyright 2022, Royal Society of Chemistry.



**Fig. 15.** (a) Top and side views of the HAB monolayer, (b) Adsorption Gibbs free energies for \*NO and \*H on various HAB monolayers, the TM atom in shaded blue and brown box can be classified into two kinds: the fourth periodic TM and the fifth periodic TM, respectively, Free-energy diagrams for NO reduction on (c) Co-HAB and (d) Rh-HAB MOFs at zero and limiting potential. Reproduced with permission [184]. Copyright 2021, Wiley-VCH.

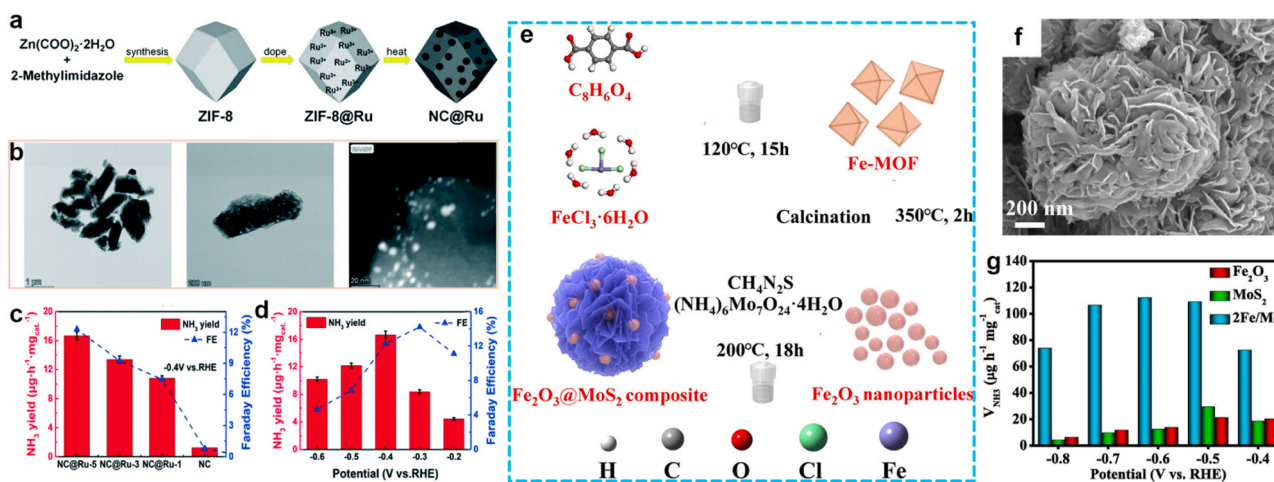
and FE value of 21.79% at  $-0.9$  V vs. Ag/AgCl). Except for the original metal species, the MOF derived metal/carbon can be employed as a template for constructing metal-doped carbon. As shown in Fig. 17a, b, Ru NPs dispersed on N-doped carbon materials were fabricated via the carbonization of Ru-doped ZIF-8 with different Ru amounts (denoted as NC@Ru-1, NC@Ru-3, NC@Ru-5,) [187]. From the transmission electron

microscope (TEM) images, Ru NPs were dispersed on the retained separate lamellar framework structure. While the NC@Ru hybrids and NC were used for electrocatalytic  $\text{N}_2$ -to- $\text{NH}_3$ , NC@Ru-5 displayed the best performance at  $-0.4$  V vs. RHE in  $0.1$  M KOH electrolyte ( $\text{NH}_3$  yield of  $16.68 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$  and FE of 14.23%) (Fig. 17c, d). This work provides a feasible approach to prepare dispersed noble metal on carbon



**Fig. 16.** (a) Schematic illustration of NPC preparation, (b) Contents of pyridinic, pyrrolic, and graphitic N in NPCs, (c) Ammonia production rates of NPC-750, NPC-850, and NPC-950 at  $-0.7$  and  $-0.9$  V vs. RHE

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**Fig. 17.** (a) The synthetic process of NC@Ru. (b) TEM images and high-angle annular dark field scanning transmission electron microscopy (HAADF-STEM) of NC@Ru-3. (c)  $\text{NH}_3$  yields and FEs of different catalysts, (d) FEs of NC@Ru at different applied potentials. (e) The synthetic approach of  $\text{Fe}_2\text{O}_3/\text{MoS}_2$ , (f) Scanning electron microscopy (SEM) image of  $\text{Fe}_2\text{O}_3/\text{MoS}_2$ , (g)  $\text{NH}_3$  yields of different samples.

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for promoting NRR activity. To further improve the catalytic activity of the derived metal, introducing foreign metal to modulate the surface charge distribution and surface structure is a good strategy. W. Huang et al. prepared  $\text{CoRu}@\text{NC}$  through encapsulating ruthenium atoms into ZIF-67 precursor, which exhibited outstanding electrocatalytic NRR activity: an  $\text{NH}_3$  yield of  $56.82 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$  and FE of 2.02% at  $-0.3$  V vs. RHE in 0.1 M KOH [189]. Except for the metal, some MOF-derived metal compounds have been also developed as efficient electrocatalysts for NRR. For example, MOF-derived  $\text{Fe}_2\text{O}_3 @\text{MoS}_2$  was reported by Ma's group recently [188]. The  $\text{Fe}_2\text{O}_3 @\text{MoS}_2$  composite was prepared through adding the Fe-MOF derived  $\text{Fe}_2\text{O}_3$  particles to the synthetic process of  $\text{MoS}_2$  (Fig. 17e). From the SEM images, we can see the  $\text{Fe}_2\text{O}_3$  NPs were anchored on the surface of nanoflower-shaped  $\text{MoS}_2$

(Fig. 17f). Electrochemical tests indicate that  $\text{Fe}_2\text{O}_3 @\text{MoS}_2$  achieves an outstanding  $\text{NH}_3$  yield of  $112.15 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$  at  $-0.6$  V vs. RHE and a high FE of 8.62% at  $-0.4$  V vs. RHE in 0.1 M  $\text{Na}_2\text{SO}_4$ , much better than those of the separate  $\text{MoS}_2$  and  $\text{Fe}_2\text{O}_3$  (Fig. 17g). The excellent performance of the  $\text{Fe}_2\text{O}_3 @\text{MoS}_2$  can be ascribed to the synergistic effect of Mo and Fe catalytic sites that activated  $\text{N}_2$  with a low energy barrier. Very recently, Dai et al. developed  $\text{TiO}_2/\text{CeO}_2$  framework with plentiful oxygen vacancies based on Ti-based MOFs MIL-125- $\text{NH}_2$  for electrochemical NRR. The unique porous framework and hetero-interfaces collectively facilitated the adsorption/activation of  $\text{N}_2$  and mass transfer [190].

Another very important kind of MOF derivatives is MOF-derived single-metal-atom catalysts (SACs) due to the high utilization of the

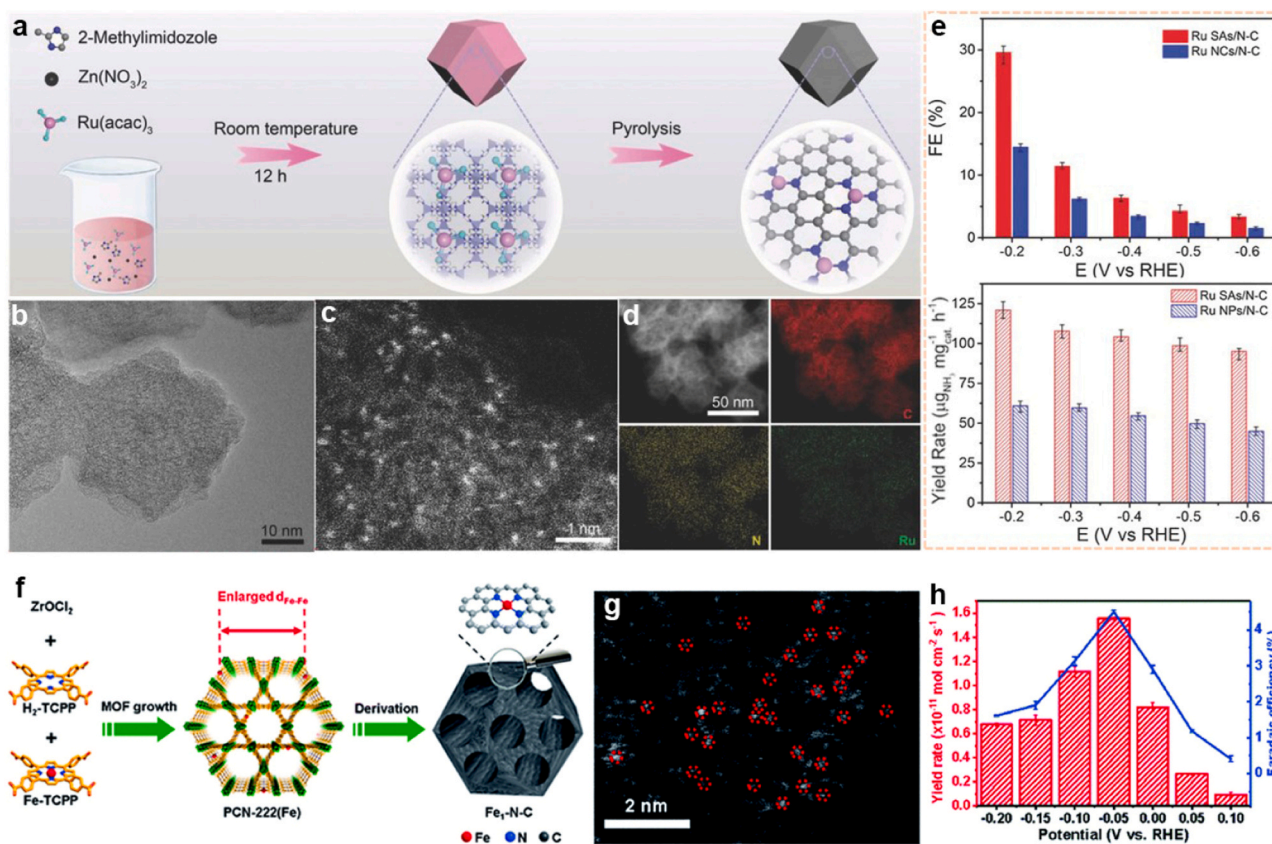


metallic catalytic site. And MOF materials are attractive precursors for preparing the dispersed SACs due to the adjustable and high dispersed metal center and the isolated metal atoms can be well stabilized by heteroatom and/or the defective sites derived from the MOF precursors. In 2018, Zeng's group first reported Ru single atoms distributed on nitrogen-doped carbon (Ru SAs/N-C) with a record-high activity for electrocatalytic  $\text{N}_2$  reduction [191]. As showed in Fig. 18a, the Ru SAs/N-C with the Ru mass loading of 0.18% was synthesized via pyrolyzing the Ru-containing derivative of ZIF-8 at 900 °C in  $\text{N}_2$  atmosphere. The morphology of the Ru SAs/NC was irregular polyhedrons and the highly dispersive Ru atoms on the N-doped carbon could be seen clearly (Fig. 18b-d). Electrocatalytic measurements demonstrate the Ru SAs/N-C showed much better activity for NRR than the Ru NPs/N-C and achieved a record-high yield rate of  $120.9 \mu\text{g h}^{-1} \text{mg}_{\text{cat}}^{-1}$  at  $-0.2 \text{ V}$  vs. RHE with the FE of 29.6% (Fig. 18e). Later, Jiang and co-authors developed the non-noble metal SAs of  $\text{Fe}_1\text{-N-C}$  via using the PCN-222 (Fe) as template during pyrolysis (Fig. 18f) [192]. From the aberration-corrected HAADF-STEM image, many isolated bright spots were found clearly in the  $\text{Fe}_1\text{-N-C}$ , suggesting the well dispersion of Fe atoms (Fig. 18g). The Fe contents in  $\text{Fe}_1\text{-N-C}$  was 1.71 wt%. The  $\text{Fe}_1\text{-N-C}$  achieved the  $\text{NH}_3$  production rate of  $1.57 \times 10^{-10} \text{ mol s}^{-1} \text{cm}^{-2}$  and FE of 4.51% at a low potential of  $-0.05 \text{ V}$  vs. RHE (Fig. 18h). These studies offer a meaningful guideline for synthesizing atomically dispersed metal catalysts through the aftertreatment of MOF precursors for efficiently electrochemical  $\text{N}_2$  conversion to  $\text{NH}_3$  the ambient conditions.

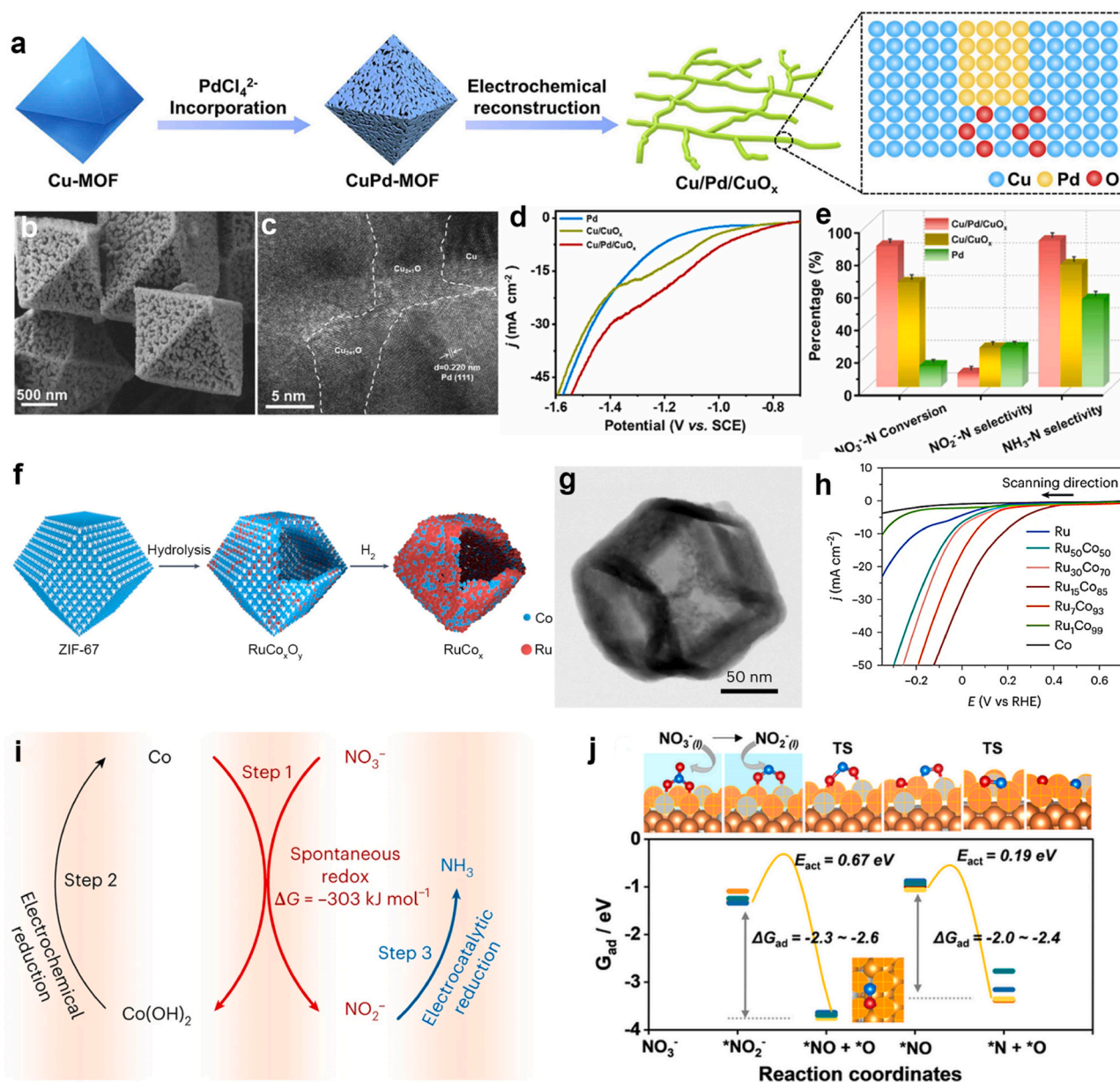
#### 4.2.2. $\text{NO}_3^-/\text{NO}_2^-$ RR

MOFs-derived metal electrocatalysts have attracted most interests for  $\text{NO}_3^-/\text{NO}_2^-$ RR due to the intrinsic activity of many metals (Cu, Co, Fe, Ti etc.) [213] and the well dispersion of MOF-derived metals. For example, Sun's team reported the adenine-based MOF derived Co NPs as

an attractive electrocatalyst for efficient  $\text{NH}_3$  synthesis from nitrate [200]. Geng et al. reported Cu NPs encapsulated with porous carbon framework (denoted Cu@C) for  $\text{NO}_3^-$ RR at ultralow concentrations. Owing to the porous structure,  $\text{NO}_3^-$  could be concentrated in Cu@C, thereby facilitating the mass transfer of  $\text{NO}_3^-$  with ultralow concentrations [201]. To further improve the active of metallic electrocatalysts, the second metal was proposed to be introduced. Xu et al. developed Cu/Pd/CuO<sub>x</sub> multi-phase heterostructures through in situ electrochemical reconstitution of Pd-incorporated Cu-based MOF for EAS [203]. The schematic illustration for the preparation of Cu/Pd/CuO<sub>x</sub> was showed in Fig. 19a, and the interfaces of Cu and Pd can be clearly observed in the HRTEM image (Fig. 19b, c). Due to the contact and the electronic interaction between Cu, Pd, the electron transferred from Pd to Cu, promoting the nitrate adsorption on electron-deficient Pd sites. And the electron-rich Cu sites further suppressed the competitive HER process. So, the Cu/Pd/CuO<sub>x</sub> exhibited the best performance compared with the corresponding contrasts (Fig. 16d, e). Additionally, Dong and co-workers fabricated a series of CuNi alloy NPs with different Cu/Ni ratio embedded in nitrogen-doped carbon matrix through the pyrolysis of Cu, Ni bimetallic MOF materials for high-efficiency electrochemical  $\text{NO}_3^-$  to  $\text{NH}_3$  [205]. The optimized CuNi/NC catalyst (Cu:Ni = 5:1) showed superior performance with the  $\text{NH}_3$  selectivity of 94.4% and FE of 79.6% and distinctly alleviate the production of toxic byproduct of nitrite. Recently, Zhang et al. synthesized a series of Ru<sub>x</sub>Co<sub>y</sub> hollow nanododecahedrons (HNDs) through the post-treatment of dodecahedral ZIF-67 (Fig. 19f, g) [204]. The LSV curves indicated Ru<sub>15</sub>Co<sub>85</sub> HNDs exhibit the highest current density at the present of  $\text{NO}_3^-$  (Fig. 19h). A novel three-step relay mechanism of nitrate reduction over Ru<sub>15</sub>Co<sub>85</sub> was proposed to overcome the issue that the high reaction overpotential was needed over most electrocatalysts. During  $\text{NO}_3^-$ RR, the three-step relay processes that involve spontaneous redox between Co and  $\text{NO}_3^-$ ,



**Fig. 18.** (a) The synthetic strategy of Ru SAs/NAC, TEM (b), HAADF-STEM (c) and corresponding elemental mapping (d) of Ru SAs/NAC, (e) FEs and  $\text{NH}_3$  yield rates of Ru SAs/NAC and Ru NPs/NAC (f) Schematic diagram of  $\text{Fe}_1\text{-N-C}$  derived from PCN-222(Fe), (g) HAADF-STEM images of  $\text{Fe}_1\text{-N-C}$ , (h) NRR properties of  $\text{Fe}_1\text{-N-C}$  (a-e) Reproduced with permission [191]. Copyright 2018, Wiley-VCH. (f-h) Reproduced with permission [192]. Copyright 2019, Royal Society of Chemistry.



**Fig. 19.** (a) Schematic illustration of the preparation of Cu/Pd/CuO<sub>x</sub>, (b) SEM and (c) HRTEM images of Cu/Pd/CuO<sub>x</sub>, (d) LSV curves and (e) NO<sub>3</sub>-N conversion efficiency, selectivity of NH<sub>3</sub>-N and NO<sub>2</sub>-N over the Cu/CuO<sub>x</sub>, Pd NNs and Cu/Pd/CuO<sub>x</sub>, (f) Schematic of Ru<sub>x</sub>Co<sub>y</sub> HND synthesis, (g) TEM image of Ru<sub>15</sub>Co<sub>85</sub>, (h) LSV curves for the NO<sub>3</sub>RR over Ru<sub>x</sub>Co<sub>y</sub> HNDs under 1600 r.p.m. with 80% iR correction, (i) The three-step relay mechanism for the NO<sub>3</sub>RR, (j) The activation and reaction energies of the N-O bond-breaking elementary steps

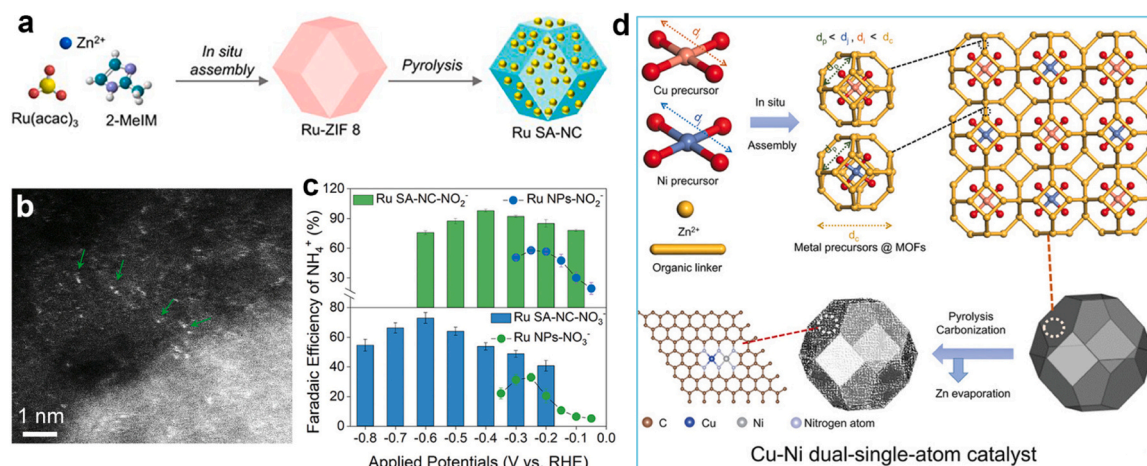
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Co(OH)<sub>2</sub> electroreduction to Co, and electrocatalytic conversion of NO<sub>2</sub><sup>-</sup> to NH<sub>3</sub> occurred (Fig. 19i). The theoretical simulations result of the catalytic reduction of NO<sub>3</sub><sup>-</sup> (aq) to NO<sub>2</sub><sup>-</sup> (aq) showed that the chemical cleavage of the N-O bond in \*NO<sub>2</sub> and \*NO is thermodynamically highly favoured on Ru<sub>15</sub>Co<sub>85</sub> (Fig. 19j).

To improve the atomic utilization of metal catalyst, atomically dispersed metal derived from MOF materials have also been explored for EAS from NO<sub>3</sub><sup>-</sup>/NO<sub>2</sub><sup>-</sup>. As an example, Xiao et al. prepared atomically dispersed Ru sites loaded on nitrogenated carbon (Ru SA-NC) by a metal organic framework assisted self-assembly process (Fig. 20a, b) [206]. The authors declared that the isolated Ru sites could promote the potential rate-limiting step of \*NO → \*NOH process, thus showed maximal FE of 97.8% (NO<sub>2</sub><sup>-</sup> to NH<sub>3</sub>) and 72.8% (NO<sub>3</sub><sup>-</sup> to NH<sub>3</sub>) toward at -0.6 and -0.4 V vs. RHE, respectively, significantly higher than those of Ru NPs (Fig. 20c). Apart from the noble metal, atomically dispersed transition

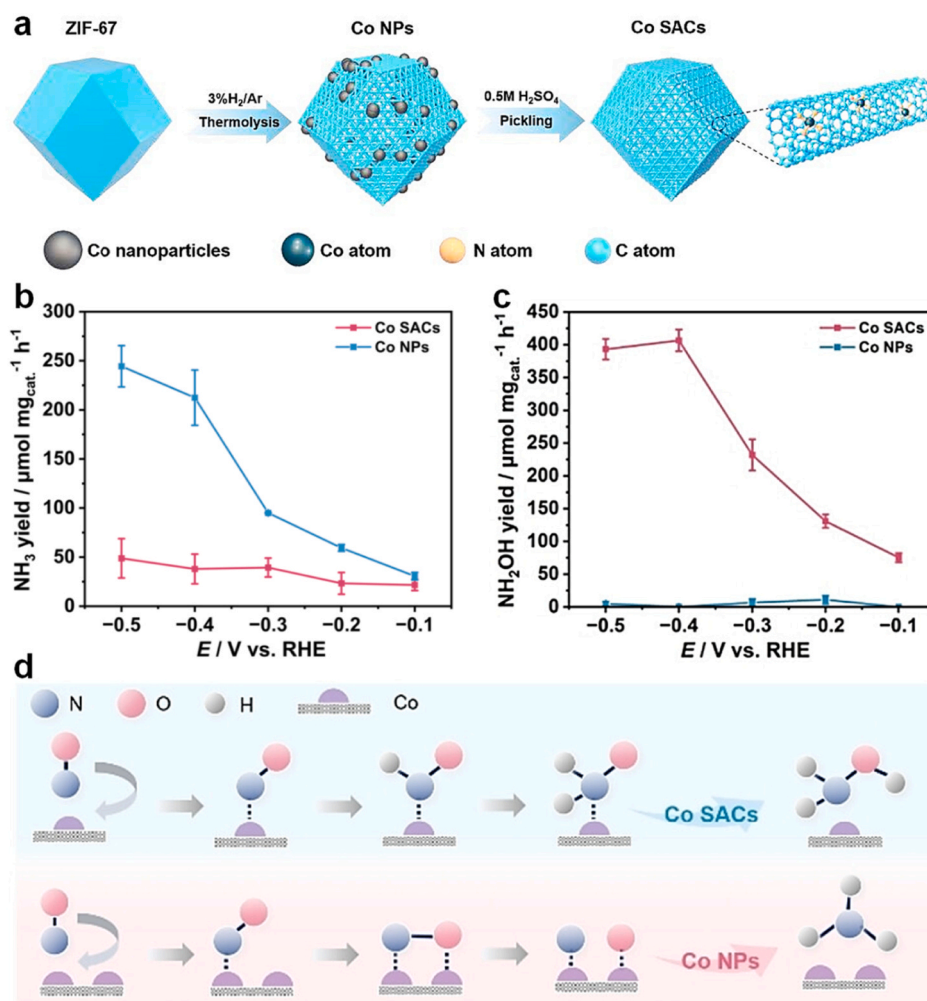
metal was fabricated through post-treatment of MOF materials for nitrate reduction. Ye and coworkers prepared atomically dispersed Cu sites on dual-mesoporous N-doped carbon matrix (Cu-N-C) by a pyrolysis treatment of Cu(acac)<sub>2</sub> @ZIF-8 for efficient EAS from nitrate [207]. Furthermore, two atomically dispersed transition metals were also successfully synthesized from corresponding MOF materials. Due to the in situ-trap Cu and Ni precursors in the cages of ZIF-8 during crystallization, Cu and Ni dual-single-atom into nitrogen-doped carbon was obtained after the pyrolysis of Cu<sup>2+</sup>, Ni<sup>2+</sup> filled ZIF-8 (Fig. 20d) [208]. The prepared Cu/Ni-NC with dual active sites shows the higher FEs (97.28%) and selectivity (94.84%) of NH<sub>3</sub> during nitrate reduction compared with Cu-NC and Ni-NC. The superior performance of Cu/Ni-NC was mainly attribute to two factors: (i) the strong hybridizations of Cu 3d - Ni 3d - O 2p orbitals of NO<sub>3</sub><sup>-</sup> can accelerate electron transfer from Cu-Ni dual-site to NO<sub>3</sub><sup>-</sup>, (ii) Cu/Ni-NC can not only





**Fig. 20.** (a) Illustration of Ru SA-NC synthesis, (b) HAADF-STEM image, (c) FEs of  $\text{NH}_3$  from  $\text{NO}_3^-$  and  $\text{NO}_2^-$  reduction over Ru SA-NC and Ru NPs (d) Schematic illustration of the synthetic procedure of Cu/Ni-NC.

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**Fig. 21.** (a) Schematic illustration of the preparation of Co SACs and Co NPs, (b) Yield rate of  $\text{NH}_3$  on Co SACs and Co NPs at each given potential, (c) Yield rate of  $\text{NH}_2\text{OH}$  on Co SACs and Co NPs at each given potential, (d) Deduced electrocatalytic NORR pathway on Co SACs and Co NPs for the production of  $\text{NH}_2\text{OH}$  and  $\text{NH}_3$ , respectively.

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decrease barrier of the rate-limiting step but also suppress N-N coupling for N<sub>2</sub>O and N<sub>2</sub> formation and HER.

#### 4.2.3. NORR

Currently, the development of MOFs-derived electrocatalysts for EAS from NO<sub>x</sub> is still in initial stage. Very recently, Zhang and coworkers developed ZIF-67 derived Co electrocatalysts for electrocatalytic NORR [210]. The product selectivity of NORR over different Co catalysts was studied in-depth. Concretely, Co SACs and Co NPs were prepared by the facile chemical conversion of ZIF-67 precursor and the schematic diagram of the synthesis process was showed in Fig. 21a. When the Co SACs and Co NPs were applied as the electrocatalysts for NORR, they showed quite different selectivity of the production. As shown in Fig. 21b, c, For Co NPs, the main product was NH<sub>3</sub>, but Co SACs selectively produced hydroxyl amine (NH<sub>2</sub>OH). In-depth exploration results by the authors unveil that linear adsorption of NO on isolated Co sites enables NH<sub>2</sub>OH formation and bridge adsorption of NO on adjacent Co sites induce the production of NH<sub>3</sub> (Fig. 21d). This work provides well scientific guidance to design efficient electrocatalysts for selective NORR to NH<sub>3</sub>.

## 5. Summary and outlook

The EAS is considered as an environmentally friendly alternative to the traditional energy-intensive H–B process. MOF-based materials are a family of promising electrocatalysts that attract great attention to act as electrocatalysts for EAS due to their unique structural merits. In this review, we summarized recent advances of the class of MOFs and their derivatives acted as electrocatalyst for EAS, including the possible mechanism of EAS via ERRs using various nitrogen sources as well as the quantification methods of ammonia, the structural features and merits of MOF-based materials acted as electrocatalysts, and recent advance in NH<sub>3</sub> synthesis from various nitrogen sources under ambient conditions over MOF-based electrocatalysts. The highly diverse and tunable structural/compositional properties endow pristine MOFs/MOF composites excellent electrocatalytic performance for EAS via ERRs using various nitrogen sources. Additionally, these advantageous properties also enable multiple rational design of MOF derivatives with high-active sites, conducive interaction in interfaces/heterostructures, porous structures to achieve a best overall electrochemical performance of ammonia synthesis, as discussed as above sections. To improve the electrocatalytic performances of MOF-based materials, constructing the multiple components with interfaces is an efficient method due to the electronic properties of the active components could be optimized by the interfacial charge redistribution. However, as displayed in Table 1 and Table 2, the NH<sub>3</sub> yield rate and FE, especially using N<sub>2</sub> as nitrogen source, are still lower than the commercially viable targets released by the U. S. Department of Energy (a current density of 300 mA cm<sup>-2</sup> with a FE of 90% and energy efficiency of 60%) over most of current reported MOF-based electrocatalysts [91]. More efforts to rationally design MOFs-based electrocatalysts and catalytic system with high current density, FE and stability for EAS are anticipated but still challenging.

Based on our current understanding of EAS based on MOFs and their derivatives, a few comments for future research in this field can be suggested.

- (1) To achieve the commercially viable targets, constructing of a new type of electrolysis reactor to realize stable and continuous NH<sub>3</sub> production with high current density is important for the practical application of EAS. And the separation and collection technology of ammonia is expected to be integrated to the electrolysis reactor. Additionally, large-scale NO<sub>3</sub><sup>-</sup> electroreduction in the actual waste water for NH<sub>3</sub> synthesis to achieve “turn waste into wealth” is still a great challenge due to the fluctuation and complexity (e.g., NO<sub>3</sub><sup>-</sup> concentration, pH value, conductivity and interference of impurity ions) of the actual waste water, which requires the ingenious design of the electrocatalysts with

selective adsorption, high activity, thermal/chemical stability for the large-scale sewage treatment.

- (2) The clear catalytic mechanism of MOFs and their derivatives for EAS via ERRs from various nitrogen sources is essential to elucidate the structure-activity relationship for adequately guiding the rational design of MOFs-based functional materials. The comprehensive utilization of multiple in situ test techniques like diffuse Fourier transform infrared spectrum (DRIFTS), Raman spectrum, differential electrochemical mass spectrometry (DEMS), and electron spin resonance (ESR) spectroscopy combined with X-ray diffraction (XRD), X-ray absorption fine structure (XAFS) and the theoretical calculations is efficient to reveal the accurate catalytic active site and reaction path. Based on the transparent catalytic mechanism, regulating and optimizing the compositions, electronic structures, and coordination environments of MOF based catalysts can efficiently decrease the highest energy barrier of rate-determining step and thus improve the catalytic performance.
- (3) The economic efficiency (EE) should be considered as one of the significant indicators of EAS performance evaluation criteria of the catalysts. For the practical application, the final cost of the electrochemical process is highly dependent on energy consumption. So, the less energy the EAS consumes, the more economical it is for sustainable application.
- (4) Considering that one of the most important applications of NH<sub>3</sub> is acted as the feedstock for amide chemicals, like urea, formamide and so on, it is fascinating that electrochemically coupling the CO<sub>2</sub> reduction and ammonia synthesis from various nitrogen sources realizes C-N bonding through precise designing MOFs or their derivatives as electrocatalysts.

In summary, MOFs and their derivatives show greatly up-and coming platforms to obtain high-efficiency electrocatalysts for the NH<sub>3</sub> synthesis via different nitrogen sources. But the current research is still in the preliminary theoretical stage and far from the standard of practical application. More efforts from chemists, electrochemists, material scientists, and chemical engineers are needed to store the renewable energy and reduce the energy consumption and CO<sub>2</sub> emissions of the NH<sub>3</sub> industry synthesis.

## Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

## Data Availability

No data was used for the research described in the article.

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